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ORIGINAL ARTICLE



Removal of microparticles and bacterial inactivation in freshwater RAS by use of foam fractionation, H_2O_2 and NaCl

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Abstract

Foam fractionation (FF) is an effective water treatment technology used to remove fine particles in seawater recirculating aquaculture systems (RAS). However, there is only limited available information on the operation and efficiency of FF in freshwater. This study investigated the treatment efficiency of FF by measuring changes in bacterial activity and microparticle densities in freshwater from RAS. Thirty-six separate batch tests were performed with FF separately and in combination with addition of hydrogen peroxide (H_2O_2) and salt (NaCl). Both chemicals are commonly used for water treatment in freshwater aquaculture. The experiment was a $2 \times 2 \times 3$ factorial design with 3 factors: FF (present or absent), H_2O_2 (0 or 10 mg L⁻¹) and NaCl (0, 3, or 10 ppt). FF reduced the concentration of microparticles and turbidity in freshwater by 58.7 \pm 5.4% and 27.5 \pm 3.8% respectively. H₂O₂ had a significant antimicrobial effect, and the combination of H₂O₂ and FF resulted in an 80% reduction in bacterial activity in freshwater. Addition of NaCl improved the efficiency of FF by further reducing particle concentration and turbidity two-fold at 10 ppt compared to 0 ppt. This study provides new knowledge on the potential use of FF to improve the water quality in freshwater RAS, and this was further enhanced by the addition of H₂O₂ or NaCl.

KEYWORDS

bacterial activity, foam fractionation, microparticle, protein skimming, RAS, water quality

1 | INTRODUCTION

Recirculating aquaculture systems (RAS) are characterized by limited water exchange, substantial feed input and associated needs for water treatment (Espinal & Matulić, 2019; Martins et al., 2010). Long retention time, accumulation of particulate matter and high levels of nutrients favour heterotrophic bacterial growth in RAS (Blancheton et al., 2013; Leonard et al., 2000; Rojas-Tirado et al., 2018). The heterotrophic bacteria colonize surfaces within the system and also constitute a substantial fraction of the microparticles in the water phase in the form of planktonic cells, multicellular bacterial aggregates or bio-flocs

(Blancheton et al., 2013; de Jesus Gregersen et al., 2019; Leonard et al., 2000; Pedersen et al., 2017, 2019). Whereas large particles are easily removed from RAS (Cripps & Bergheim, 2000; Piedrahita, 2003), microparticles are difficult to remove by traditional mechanical processes, and they, therefore, accumulate (Fernandes et al., 2017; Patterson et al., 1999). Direct and indirect impacts of these particles on fish performance and RAS operation have recently been described (Becke et al., 2020; Schumann & Brinker, 2020). Recent aquaculture studies have demonstrated methods to control and remove the waterborne bacterial load by removing microparticles or inactivating bacteria (Bentzon-Tilia et al., 2016; Fossmark et al., 2020; Huyben et al., 2018;

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de Jesus Gregersen et al., 2020; Wold et al., 2014). However, there is still a need to test and develop alternative, simple and cost-effective water treatment methods that can improve water quality in RAS.

One effective water treatment technology is foam fractionation (FF), a treatment that has been applied in various industries for decades (Burghoff, 2012; Timmons & Losordo, 1994). Foam fractionation or protein skimming is a physical-mechanical process that extracts dissolved and particulate matter from the water phase into foam. The treatment efficiency of FF depends on several factors, such as the air bubble diameter, the air-to-water ratio, the concentration and charge of dissolved compounds and solids, the retention time of the water in the reactor, the surface tension and the interaction of the surfactants to produce foam (Brambilla et al., 2008; Park et al., 2015; Wilson et al., 2001). The process of FF is well described (Lekang, 2020; Summerfelt, 1999; Timmons & Losordo, 1994), and the potential use of FF in aquaculture has been evaluated (Brambilla et al., 2008; Chen et al., 1994; French et al., 2000; Landau et al., 2002; Park et al., 2015; Peng et al., 2003). So far, FF is mainly applied in saltwater RAS (Colt & Huguenin, 2002), with limited information about FF application in freshwater aquaculture. The limited or absent use of FF in freshwater is primarily associated with a suboptimal removal efficiency due to larger bubble sizes and less surface tension compared to seawater. Recent studies have shown that ozone can improve FF treatment efficacy in seawater (Figueiras Guilherme et al., 2020; Park et al., 2015), although using ozone is challenging due to its toxicity and safety issues for fish and staff (Bregnballe, 2015). Hydrogen peroxide (H_2O_2) is a milder alternative to ozone with similar characteristics (i) can be used to oxidize organic matter (Cuerda-Correa et al., 2020) (ii) is easily degradable, (iii) do not form harmful by-products (Schmidt et al., 2006) and (iv) is commonly applied in aquaculture systems (Arndt & Wagner, 1997; Bögner et al., 2020; Pedersen & Pedersen, 2012; Rach et al., 1998; Saez & Bowser, 2001). Salt (NaCl) is also widely used in freshwater fish farms as an anti-parasitic treatment (Aihua & Buchmann, 2001; Jørgensen et al., 2009; Lahnsteiner & Weismann, 2007), and it increases the surface tension of the water.

The current study investigated the potential use of FF to improve water quality in freshwater RAS. The performance of FF in RAS water was tested by measuring bacterial activity (Pedersen et al., 2019) and the density of microparticles (de Jesus Gregersen et al., 2019) to evaluate its effects on water quality. This study also investigated whether the efficiency of FF could be improved by adding either H_2O_2 or NaCl, or combinations of the two.

2 | MATERIALS AND METHODS

The experiments were performed at the Section for Aquaculture, DTU Aqua, in Hirtshals, Denmark.

2.1 | RAS water

Water for the experiments was collected from a pilot-scale freshwater RAS operated for several months in steady-state at 16°C. The system included an 8.5 m³ rearing tank stocked with approx. 200 kg of rainbow trout (*Oncorhynchus mykiss*) fed 1.0 kg of commercial feed daily and with a water renewal rate of 1.0 m³/d. In addition, the system included two 0.40 m³ fixed bed and two 0.40 m³ submerged bio-filters, and a trickling and a drum filter (Pedersen et al., 2015). The water was collected from the outflow of the rearing tank early in the morning before the feeding commenced.

2.2 | Experimental design

Individual batch tests with 20 L RAS water were conducted in 30 L tanks (dimensions: Height = 37 cm, depth = 30 cm, width = 27 cm). Each tank was equipped with a pump (Tunze Silence 1073.008, Tunze Aquarientechnik GMBH, Germany) to ensure mixing of the water, a foam fractionator (Delaman® Protein Skimmer para Acuario Marino, size N°1, MN-27220-SE1, Amazon). The FF used was 28 cm high, and the air was supplied from the bottom using a wooden air stone (Sander No. 2, Erwin Sander Elektroapparatebau GmbH, Germany). The foam produced by the FF was collected by overflow into 2 L plastic bottles.

The experimental design included 3 factors (Figure 1): presence or absence of FF; H_2O_2 (0 or 10 mg $H_2O_2 L^{-1}$) and NaCl (salinity of 0, 3, or 10 ppt). Salinity was adjusted by adding sea salt (Sea Salt,



FIGURE 1 Conceptual sketch of the 3-factorial design experiment. Each treatment (n = 12) was conducted in triplicates in containers with 20 L RAS freshwater (N = 36). Samples were collected at time 0 and after 6 h

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Aquaforest, Poland) in the RAS water before it was transferred into the experimental tanks (20 L in each). Each experimental trial lasted 6 h and samples were collected just prior to treatment (t = 0 h) and at the end of the trial based on preliminary trials. A total number of 36 batch experiments were performed over a period of three consecutive days.

2.3 | Sampling and analysis

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Samples were collected and handled uniformly prior to the start and after 6 h of treatment. Turbidity was measured with a portable handheld turbidity meter (Hach 2100Q, Hach, United States). Particle concentration (# mL⁻¹) of particles ranging between 5.6 and 160 μ m in diameter, was measured with a Coulter Counter (Multisizer 4e Coulter Counter, Beckman Coulter Life Science, US). The amounts of organic matter removed as foam (foamate) from the water by FF were analysed for total suspended solids (TSS) and total chemical oxygen demand (TCOD). TCOD (mg O₂ L⁻¹) was measured using two sets of test kits (LCK 314, LCK 1414; Hach, United States). TSS (mg L⁻¹) was quantified according to APHA standard method 2005.

The per cent removal efficiency measured as TSS and TCOD was calculated according to Eq. (1):

$$RE(\%) = \frac{C_f \times V_f}{C_o \times V_w} \times 100$$
(1)

where RE is the removal efficiency (%), C_f is the concentration (TSS or TCOD) in the foamate, V_f is the total foamate volume (L), C_0 is the initial concentration (TSS or TCOD) in the water, and V_W is the initial water volume (L).

The bacterial activity in raw water samples was determined according to the hydrogen peroxide degradation method (Pedersen et al., 2019). This assay relies on the quantification of the enzymatic degradation of H_2O_2 under constant conditions, which is calculated as a degradation rate constant *k* (h⁻¹) based on Eq. (2):

$$C_t = C_0 \times e^{-kt} \tag{2}$$

where C_t and C_0 is the H₂O₂ concentration at time t and 0 respectively.

2.4 | Data analysis

The concentration of microparticles, turbidity and bacterial activity were normalized as per cent of measurements at time zero using formulae (3):

% remaining =
$$\frac{Value \ at \ time \ t}{Value \ at \ time \ 0} * 100$$
 (3)

The data were normalized to facilitate comparison between treatments at the end of the experiment and to correct TABLE 1 Range of selected RAS water quality parameters used for the batch experiments over three days. Measurements were done prior to the treatments (t = 0)

Variables	Range
Temperature	15.0-16.5
pН	7.4-7.8
Oxygen conc. (mg $O_2 L^{-1}$)	>9
Bacterial Activity (k (h^{-1})	0.16-0.47
Particle numbers (# mL ⁻¹)	1.21-1.70·10 ⁵
Turbidity (NTU)	4.4-5.8

for differences in start conditions for replicated experiments. A summary of the measured variable range at time zero is listed in Table 1. Data are presented as average \pm SD. A three-way ANOVA was conducted to compare the main effects of foam fractionation, hydrogen peroxide and salinity and interaction effects. Differences in treatment means were tested by Tukey's post hoc test with a pre-defined significance level of p < 0.05. Statistical analyses were made using SPSS version 25.

2.5 | Ethics statement

The experiments conducted in this trial did not need any ethical approval, as no animals were used during the trial.

3 | RESULTS

3.1 | Bacterial activity

For the control treatment, the bacterial activity in the water increased after 6 h incubation (Figure 2a). In general, FF reduced bacterial activity and the addition of salt significantly lowered bacterial activity when comparing 10 and 0 ppt treatments (Figure 2a). The addition of H_2O_2 significantly reduced bacterial activity by 69.5 ± 5.3% at the three salinities tested (p < 0.001). When H_2O_2 was combined with FF, a further significant reduction in bacterial activity was observed. On average, at all three tested salinities the bacterial activity was 58% lower when H_2O_2 was combined with FF compared to H_2O_2 addition only (Figure 2a, Table 2).

3.2 | Microparticle concentration and turbidity

FF significantly reduced particle numbers and turbidity (p < 0.001, Figure 2b,c and Table 2). The average number of microparticles was 74.2 \pm 4.1% lower and turbidity was 42.9 \pm 3.7% lower in the FF treatments compared to control treatment without FF (Figure 2b,c). H₂O₂ addition did not affect particle numbers or turbidity (p = 0.709and 0.184 respectively). Increased salinity significantly reduced both **FIGURE 2** Relative changes in selected water quality variables after 6 h of treatment compared with start values; (a) bacterial activity, (b) particle concentration and (c) turbidity. The treatment combinations included foam fractionation (FF) vs. control (no FF); hydrogen peroxide (10 mg $H_2O_2 L^{-1}$) vs. control (no H_2O_2) and salinity (0, 3, or 10 ppt). The data presented (mean \pm SD; n = 3) reflects normalized value calculated according to each group's initial values before treatment (t = 0). The different letter denotes significant differences between groups (p < 0.05)



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TABLE 2 Three-way analysis of variance (ANOVA) of different water riables

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	494.84	. ,
	< 0.001	

Treatments	parameters	activity	concentration	Turbidity
FF ^a	F	30.392	766.40	494.84
	p-value	<0.001	<0.001	<0.001
	Effect size ^b	0.559	0.970	0.954
H ₂ O ₂	F	354.886	0.709	1.871
	p-value	<0.001	0.142	0.184
	Effect size	0.937	0.006	0.072
Salinity	F	3.211	11.92	20.84
	p-value	0.058	<0.001	<0.001
	Effect size	0.211	0.498	0.635
Interaction(FF \times H ₂ O ₂ \times salinity)	F	1.22	1.063	0.774
	p-value	0.311	0.361	0.473
	Effect size	0.093	0.081	0.061
Interaction (FF ×salinity)	F	0.657	12.744	29.27
	p-value	0.528	< 0.001	<0.001
	Effect size	0.052	0.515	0.709
Interaction (FF \times H ₂ O ₂)	F	1.781	0.398	0.657
	p-value	0.195	0.534	0.426
	Effect size	0.069	0.016	0.027
Interaction ($H_2O_2 \times salinity$)	F	2.66	1.858	0.777
	p-value	0.09	0.178	0.474
	Effect size	0.182	0.134	0.060

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^aFoam Fractionation

^bPartial Eta Squared from SPSS reported as Effect size.

particle number and turbidity when combined with FF (p < 0.001, Table 2).

3.3 TSS and TCOD collected in the foamate

The organic matter removed from the water and collected as foamate ranged from 192–365 mg L^{-1} TSS and from 266 – 648 mg O_2 L^{-1} Total COD. This was also evident when calculated as the removal percentage of TSS and TCOD from the tanks (Figure 3). TCOD and TSS removal was improved with the addition of H₂O₂ compared to FF without H₂O₂ (Figure 3, Table 3). Salinity significantly improved the removal of TSS (from $29.3 \pm 8.6\%$ in 0 ppt to $60.8 \pm 13.7\%$ in 10 ppt, p = 0.003) and TCOD (from 19.7 \pm 3.6% in 0 ppt to 32.1 \pm 4.7% in 10 ppt, p < 0.001) regardless of the presence of H₂O₂ (Figure 3).

4 DISCUSSION

The ability of FF to improve water quality by the removal of heterotrophic bacteria and particulate matter has been documented in seawater (Barrut et al., 2013; Brambilla et al., 2008; Peng & Jo, 2003; Peng et al., 2003) but not in freshwater. Performance of FF was examined in the freshwater, obtained from a pilot-scale RAS with rainbow trout, feed loading and retention time, reflecting commercial

operation. The small-scale batch tests allowed guantification of the efficacy of FF with and without the addition of sodium chloride and hydrogen peroxide by measuring changes in several water quality variables.

4.1 | Foam fractionation removes microparticles and improves water transparency

FF significantly reduced the particle concentration by 58.7 \pm 5.4% and improved turbidity in freshwater (27.5 \pm 3.8%) compared to control treatments without FF. The microparticle concentration $(1.4 \cdot 10^5 \pm 0.2 \cdot 10^5)$ included particles above 5 µm and concentrations are representative for what is found in RAS (Fernandes et al., 2017; de Jesus Gregersen et al., 2019). Microparticles accumulate in RAS and represent a significant source of bioavailable organic matter (de Jesus Gregersen et al., 2020; Pedersen et al., 2017), which FF potentially can harvest and remove from the water. Even though FF is considered less efficient in freshwater due to the lower density and surface tension of freshwater compared to seawater, the results of our experiment indicate that FF would be an effective way to remove particles and bacteria and thereby improve the water quality also of freshwater.

Bacterial activity in the water was reduced by FF treatment alone. However, the effectiveness was significantly increased by the



FIGURE 3 Percent removal efficiency of organic matter from the water as foamate after 6 h in the six treatments with FF; a) TSS and b) Total COD, (mean \pm SD; n = 3). Treatments include salinity in three levels (0, 3 or 10 ppt) and the presence (H₂O₂) or absence of hydrogen peroxide (No H₂O₂). The different letters denote significant differences between groups (p < 0.05)

addition of H_2O_2 and salt. This can be explained by the ability of salt to improve FF removal efficiency of particles and, consequently, particle-associated and free-living bacteria from the water. This result agrees with the findings of Brambilla et al. (2008), showing that removal of heterotrophic bacteria (32 to 88%) was achieved by FF in seawater. Similarly, Rahman et al. (2012) who investigated the effect of FF on bacterial abundance and abalone growth, found a lower mean bacterial abundance in water treated with FF than in untreated water, thereby confirming the efficiency of FF for the removal of bacteria from seawater.

4.2 | Hydrogen peroxide reduces bacterial activity

Bacterial activity was significantly lower in water treated with H_2O_2 than in untreated water. This reduction most likely reflects

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TABLE 3Two-way analysis of variance (ANOVA) of differentvariables in the foamate

Treatments	Statistical parameters	TSS	Total COD
H ₂ O ₂	F	1.105	12.63
	p-value	0.314	0.004
	Effect size ^a	0.084	0.513
Salinity	F	9.63	37.78
	p-value	0.003	< 0.001
	Effect size	0.616	0.863
Interaction (H ₂ O ₂ ×salinity)	F	0.159	1.095
	<i>p</i> -value	0.855	0.366
	Effect size	0.026	0.154

^aPartial Eta Squared from SPSS reported as Effect size.

the biostatic effects of H_2O_2 and the oxidative damage to relevant bacterial enzymes (Linley et al., 2012; Schmidt et al., 2006). The bacterial activity was further reduced by combining H_2O_2 and FF (average 58%) compared to the treatments without FF. This could reflect the combination of microparticle removal by FF, along with the oxidative and direct antimicrobial actions of H_2O_2 (Block, 2001). H_2O_2 addition apparently did not affect particle removal by FF. However, only microparticles with sizes above 5 μ m were measured, excluding most of the free-living bacteria (de Jesus Gregersen et al., 2020). The results presented here indicate a beneficial effect of the combination of H_2O_2 and salinity (especially 10 ppt) for particle removal by the skimming process, even with only 6 h contact time. However, these findings and the interactions between FF, $H_2O_{2 \text{ and}}$ salinity were not statistically significant and require further research.

4.3 | Addition of sodium chloride improves foam fractionation

Increased salinity in the FF treatments significantly improved the FF removal efficiency in terms of reduction in particle concentration and turbidity. According to Colt and Huguenin (2002), foam fractionation performance depends on water composition, surface tension, salinity, bubble size among others. Salt addition improved FF removal efficiency by increasing the surface tension of the water, and smaller bubbles were observed during the trial. Chen et al. (1994) showed mathematically, that reducing bubble size increased the solids removal efficiency of foam fractionators. The effect of salt addition on bacterial activity depended on the presence of FF, as salinity alone did not significantly affect the bacterial activity. This suggests that the salt simply increased the efficiency of FF, resulting in an improvement in the removal of bacteria from the system and not killing them. FF treatments without H₂O₂ substantially lowered bacterial activities at 10 ppt salinity, indicating that salinity is an important factor for particle and particle-associated bacteria removal. Aquaculture Researc

This result, an increase in the efficiency with increasing NaCl addition, further supports the theory of increased efficiency of FF at higher salinities.

5 | CONCLUSION

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With a batch setup, it was demonstrated that FF reduced the fine particle concentration and improved the turbidity of freshwater RAS. The addition of hydrogen peroxide alone had a significant antimicrobial effect and reduced the bacterial activity, while the combination of FF with hydrogen peroxide further reduced the bacterial activity. The addition of a low concentration of salt (3 and 10 ppt) improved the particle removal process during foam fractionation, and the interaction effect of FF and salinity was statistically significant. The combination of hydrogen peroxide and 10 ppt salinity during FF further improved the particle removal.

The results presented in this study stressed that simple and lowtech solutions, such as foam formation, could be applied to circumvent the problem with accumulating bacteria and organic matter in freshwater RAS. These findings may encourage further testing and development of potential long-term operation and affordable solutions to remove dissolved and particulate organic matter by foam fractionation in freshwater RAS.

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AUTHORS' CONTRIBUTION

L.F.P. and K.J.J.G., conceived the research idea, L.F.P. K.J.J.G., O.V. and L.J. designed the experimental trial. L.J. conducted the experiments, collected the samples and performed the laboratory analyses. L.J., L.F.P. and K.J.J.G. processed and analysed the data. L.J wrote the first version of the manuscript, and all authors contributed to the writing and review of the final manuscript.

CONFLICT OF INTEREST

Authors have no conflict of interest to disclose.

DATA AVAILABILITY STATEMENT

All data utilized for this trial and to support the findings are available within the article.

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