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Title: Comparing the primary energy and phosphorus consumption of soybean and seaweed-based aquafeed proteins - A material and substance flow analysis

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Corresponding Author: Mr. Gaspard Philis,

Corresponding Author's Institution: Norwegian University of Science and Technology

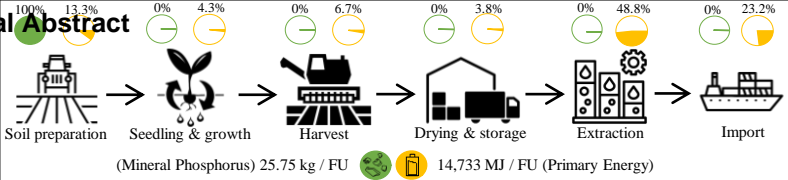
First Author: Gaspard Philis

Order of Authors: Gaspard Philis; Erik O Gracey; Lars C Gansel, Associate Professor; Annik Magerholm Fet, Professor; Céline Rebours, Senior Researcher

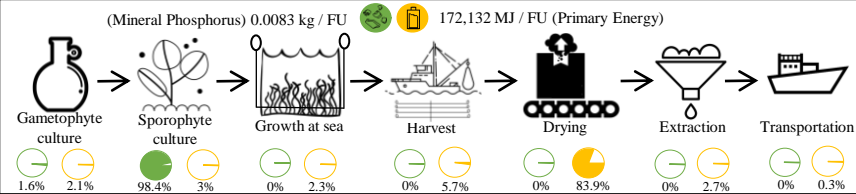
Abstract: This study compares the environmental performances of two protein sources for aquafeed production: Brazilian soy protein concentrate and Norwegian seaweed protein concentrate. The efficiency and sustainability of these two production systems are assessed using a comparative material and substance flow analysis accounting for the transfers of primary energy and phosphorus. The primary energy and phosphorus demand of 1 t of soy protein is compared to 2 t seaweed protein to assess commodities with similar protein contents. The primary energy consumption of the latter protein source (172,133 MJ) is found 11.68 times larger than for the soy-based concentrate (14,733 MJ). However, the seaweed protein energy requirement can be reduced to 34,010 MJ if secondary heat from a local waste incineration plant is used to dry the biomass during the late-spring harvest. The seaweed system outperformed the soy system regarding mineral phosphorus consumption since 1 t of soy protein requires 25.75 kg mineral phosphorus while 2 t of seaweed protein require as little as 0.008 kg input. These results indicate that substituting soy protein with seaweed protein in aquafeed leads to an environmental trade-off. The seaweed value chain produces proteins with near zero mineral phosphorus consumption by using naturally occurring marine phosphorus while the soy value-chain produces proteins for roughly 1/12th of the primary energy required by seaweed. Based on the current production technology, the seaweed value-chain will require extensive innovation and economies of scale to become energy competitive. Further research should investigate the predictive environmental impacts of a fully developed seaweed protein concentrate value-chain and account for the background emissions and multi-functionality in each system.

Graphical Abstract

Soy Protein Concentrate value-chain



Seaweed Protein Concentrate value-chain



Abstract

This study compares the environmental performances of two protein sources for aquafeed production: Brazilian soy protein concentrate and Norwegian seaweed protein concentrate. The efficiency and sustainability of these two production systems are assessed using a comparative material and substance flow analysis accounting for the transfers of primary energy and phosphorus. The primary energy and phosphorus demand of 1 t of soy protein is compared to 2 t seaweed protein to assess commodities with similar protein contents. The primary energy consumption of the latter protein source (172,133 MJ) is found 11.68 times larger than for the soy-based concentrate (14,733 MJ). However, the seaweed protein energy requirement can be reduced to 34,010 MJ if secondary heat from a local waste incineration plant is used to dry the biomass during the late-spring harvest. The seaweed system outperformed the soy system regarding mineral phosphorus consumption since 1 t of soy protein requires 25.75 kg mineral phosphorus while 2 t of seaweed protein require as little as 0.008 kg input. These results indicate that substituting soy protein with seaweed protein in aquafeed leads to an environmental trade-off. The seaweed value chain produces proteins with near zero mineral phosphorus consumption by using naturally occurring marine phosphorus while the soy value-chain produces proteins for roughly 1/12th of the primary energy required by seaweed. Based on the current production technology, the seaweed value-chain will require extensive innovation and economies of scale to become energy competitive. Further research should investigate the predictive environmental impacts of a fully developed seaweed protein concentrate value-chain and account for the background emissions and multi-functionality in each system.

1 **Keywords**

2 Aquaculture, Feed, Soybean, Seaweed, Protein, Sustainability.

4 **Abbreviation**

5 CPED Cumulative Primary Energy Demand

6 LCA Life Cycle Assessment

7 MFA Material Flow Analysis

8 SFA Substance Flow Analysis

9 P Phosphorus

10 SPC Soy Protein Concentrate

11 SWPC Seaweed Protein Concentrate

13 **1. Introduction**

14 Eradicating malnutrition and hunger is a critical task of the 21st century, and it is also the
15 second target of the sustainable development goals adopted by the United Nations on
16 September 25th, 2015 (United Nations, 2015). As the earth's population steadily marches
17 towards 9 billion by 2050, the growing demand for fiber, food, and bio-energy, overflows
18 earth's planetary boundaries (Steffen et al., 2015). Increase incomes in some of the most
19 populated countries is expected to drive demand for protein-rich food, adding pressure on the
20 biosphere (Wu et al., 2014). Erosion, deforestation and the extensive use of fertilizers in
21 agriculture are leading to a steady decline of arable land (FAO, 2011), and significant
22 disruptions of nitrogen and P cycles (Bouwman et al., 2009). This escalating discharge of
23 nutrients from land to oceans leads to eutrophication of freshwater and marine ecosystems
24 and depletes mineral Phosphorus (P) reserves (Cordell and White, 2011; Rabalais et al.,
25 2009).

26 In Norway, intensive production of farmed salmon is facing multiple environmental
27 challenges, including parasite and disease outbreaks, feed ingredient scarcity, nutrient
28 discharge, and as a result, concerns about environmental impacts are strong (Cole et al.,
29 2009). Life Cycle Assessment (LCA) results show that salmon feed is driving the
30 environmental impacts of salmon aquaculture (Hognes et al., 2014; Pelletier et al., 2009).

31 Norwegian aquafeed manufacturers started substituting large percentage of fishmeal with Soy
32 Protein Concentrate (SPC) extracted from *Glycine max* beans a little over a decade ago
33 (Ytrestøyl et al., 2015). Today, 94% of the SPC used in Norway originate from Brazil
34 (Lundeberg and Grønlund, 2017). The Brazilian soy industry is responsible for massive
35 deforestation, ecosystem degradation, resource depletion and greenhouse gas emissions in
36 one of the world's most biodiverse regions (Gibbs et al., 2015).

37 While environmental impacts associated to production are unavoidable, solutions exists to
38 produce sustainable food using efficient and innovative supply-chains causing a minimum of
39 environmental damages. Strategies suggested for mitigating climate change and reach
40 sustainable food security are based on both supply and demand transformations. The supply-
41 based strategy consists of reducing food waste and promoting the development of sustainable
42 new food supply chains (Garnett, 2014). One such platform designed for optimized
43 sustainability is the biorefinery, recently recognized by the Norwegian Research Council as a
44 key transformation unit for promoting new feed and food value chains (The Research Council
45 of Norway, 2013). Norway's extensive coastline, excellent mariculture conditions, and large-
46 scale aquaculture industry provide an excellent starting point for macroalgae cultivation as a
47 high-quality feedstock for new Norwegian biorefineries (Skjeremo et al., 2014; Stévant et al.,
48 2017).

49 Researchers are looking for sustainable alternatives to Brazilian SPC and seaweed is one of
50 the alternative feedstock considered (Sørensen et al., 2011; Ytrestøyl et al., 2015). LCA
51 research has already documented the environmental impacts of soy protein products (e.g.,
52 Dalgaard et al., 2008; Raucci et al., 2015) and Seaweed Protein Concentrate (SWPC)
53 (Seghetta et al., 2016). However, these studies were performed separately. An in-depth,
54 comparative environmental system analysis of these two value-chains is absent from the
55 scientific literature.

56 The Material Flow Analysis (MFA) and Substance Flow Analysis (SFA) methodology was
57 successfully applied in various industrial sectors to measure crucial environmental efficiency
58 indicators and to track critical substances in value-chains (Barles, 2009; Wang et al., 2016). It
59 comprises studies tracking key nutrients in agriculture (Cooper and Carliell-Marquet, 2013)
60 and aquaculture (Hamilton et al., 2015a) production systems. This study consequently applies
61 the MFA/SFA methodology to compare the primary energy and P demand of SPC (derived
62 from Brazilian *Glycine max*), and SWPC (extracted from Norwegian *Saccharina latissima*).
63 This research aims to increase the understanding of the SPC and SWPC value chains,

64 compare their environmental efficiencies across two key indicators (primary energy and P),
65 and assess the potential of SWPC as an alternative aquafeed ingredient for the Norwegian
66 aquaculture industry. Because our primary objective is to develop a deep comprehension of
67 the flow dynamics of these two production systems, we purposely used the MFA/SFA
68 methodology instead of a comparative LCA. This allows us to analyze in depth the processes
69 of each foreground systems and focus on value-chain over product comparison. A
70 comparative LCA will be performed under the PROMAC research project at a later stage to
71 supplement this environmental assessment.

73 **2. Methods**

74 **2.1. Material and Substance Flow Analysis**

75 MFA/SFA is an environmental accounting tool used to assess flows and stocks of material,
76 energy, and substance in socio-economic systems. It uses the fundamental principle that
77 neither matter nor energy can be created or destroyed in an isolated system. Their quantities
78 remain constant in a system delimited by boundaries of space and time and follow the mass-
79 balance principles (Brunner and Rechberger, 2003). In practice, the MFA/SFA involves
80 consequential modeling of anthropogenic foreground systems and is particularly useful for
81 improving resource management (Brunner, 2012). Primary modeling and flow calculations
82 were performed in Microsoft Excel while secondary modeling was performed in eSankey.

83 **2.2. The SPC and SWPC production systems**

84 Both the SPC and SWPC systems integrate cradle-to-customer gate system boundaries. In the
85 SPC system, the boundaries start with soybean cultivation in Brazilian farms and end upon
86 delivery at the factory gates of Norwegian fish feed producers, before incorporation into
87 compound aquafeed. The boundaries of the SWPC system start at a local seaweed farm
88 located in Solund, on the west coast of Norway, and end with the delivery of SWPC to a
89 Norwegian aquafeed producer. The processes of the SPC and SWPC systems were selected
90 based on primary data sources, systems understanding, and modeling assumptions (Fig. 1).

91 **< insert Fig1 here >**

92 Fig. 1: Description of SPC and SWPC processes.

93 **2.3. Model construction**

94 The life cycle inventory of Da Silva et al. (2010) was the primary data source used to model
95 soybean cultivation in Brazil. The extraction of Brazilian soybeans into SPC was modeled
96 after process data from the Agri-footprint LCA database used in Hognes et al. (2014). SPC
97 manufacturers (Caramuru, Selecta, Imcopa) and aquafeed producers (EWOS, Biomar,
98 Skretting) provided the logistics data necessary to model the import of SPC to Norway.
99 Primary cultivation data (provided by the Dutch company Hortimare), was used to construct
100 processes 1 to 3 in the seaweed system (Van Den Heuvel, F., Hortimare, Pers. Com.,
101 December 8th, 2016). Additional data describing the extraction of seaweed into SWPC was
102 gathered from the life cycle inventory of Seghetta et al. (2016) and used to model biorefinery
103 extraction. Finally, assumptions were made to build a transport scenario between the
104 hypothetical SWPC biorefinery and a local aquafeed producer (additional data).

105 The production volume of the two systems were adjusted to reach protein equivalency. This
106 adjustment ensures functional unit coherence and safeguards the comparative integrity of the
107 system requirement needed to produce the desired output; protein. Protein equivalency was
108 practically obtained by setting the functional unit of production at 1 t with 62% protein
109 content for SPC (Hognes et al., 2014), and 2 t with 31% protein content for SWPC (Seghetta
110 et al., 2016). Both functional unit contain 0.62 t of pure proteins. To respect the system's
111 mass balance, each flow of primary energy has a corresponding outflow of energy emissions.
112 Primary energy inflows and their corresponding emission outflows are equal. However, it
113 should be noted that the energy is in different states. Energy emissions are either kinetic,
114 chemical, or thermal. Tables 1 and 2 shows how the SPC and SWPC models were
115 constructed by presenting each flow's mathematical formula and corresponding data sources.
116 Energy emission flows formulas are not shown as they are identical to the primary energy
117 inflows. The full list of assumptions made during modeling is available in the additional data.

118 < insert Table 1 here >

119 < insert Table 2 here >

121 **3. Results**

122 **3.1. Current imports**

123 In 2015, Norway imported 362,217 t of SPC from a resource base of 711,673 t of soybeans,
124 generating 976,240 t of crop residues. For an average soybean yield of 2,713 kg/ha (Da Silva
125 et al., 2010), the 2015 SPC import to Norway required 1,970,247 ha of Brazilian land,

126 corresponding to the occupation of 19,702 km² of arable land. This surface represent roughly
127 ½ of the Netherlands. Norwegian SPC imports in 2015 required 5,336,705 GJ of energy,
128 which is equivalent to 1.48 TWh of primary energy, mainly in the form of fossil fuels. The
129 SPC production also required 86,626 t of mineral fertilizers, 154,675 t of manure, and
130 976,240 t of crop residues for soil enrichment. Mineral fertilizers are by far the most common
131 P input to SPC production, totaling 3,417 t of pure mineral P.

3.2. Primary energy comparative analysis

132 The Cumulative Primary Energy Demand (CPED), demonstrates significant differences
133 between the two productions systems (Fig. 2 and 3). 1 t of SPC requires 14,733 MJ of
134 primary energy while 2 t of SWPC requires 172,133 MJ of energy input. The SPC MFA/SFA
135 model (Fig. 6) indicates that primary energy requirements concentrate around the extraction
136 process (F0,5a; F0,5b) and the import to Norway (F0,6a; F0,6b; F0,6c), representing
137 combined 71.99% of the system CPED (Fig. 2). For the SWPC system (Fig. 7), primary
138 energy demand for drying the biomass eclipses all the other flows (F0,5a), representing alone
139 80.24% of the system CPED (Fig. 3).

< insert Fig2 here >

Fig. 2: Process CPED of the SPC system (MJ)

< insert Fig3 here >

Fig. 3: Process CPED of the SWPC system (MJ)

145 The distribution of primary energy use based on the type of energy (fossil and non-fossil)
146 shows that the SPC and the SWPC system have opposing energy profiles (Fig. 4 and 5). The
147 SPC system relies mainly on energy from fossil origin while the SWPC value-chain requires
148 mostly non-fossil electricity. For the SPC system, the ratio of fossil/non-fossil is 83/17%,
149 while the corresponding ratio for the SWPC system is 9/92%.

< insert Fig4 here >

Fig. 4: Process CPED of the SPC system, displayed per energy types (MJ)

< insert Fig5 here >

Fig. 5: Process CPED of the SWPC system, displayed per energy types (MJ)

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< insert Fig6 here >

Fig. 6: MFA/SFA Sankey diagram of the SPC production system

< insert Fig7 here >

Fig. 7: MFA/SFA Sankey diagram of the SWPC production system

158 **3.3. Phosphorus comparative analysis**

159 P inflows into the SPC system are dominated by mineral fertilizers (F0,1a) and crop residues
160 (F0,1c) from the previous harvest (Fig. 6). Manure (F0,1c) provides only a marginal P input.
161 Most of the total P input is either captured by *Glycine max* or fixed in the soil (F0,1b). In the
162 SWPC system, P flows are marginal until seaweed sporophytes begin to take up P from the
163 marine environment (F0,3c). According to the assumptions and biorefinery extraction
164 techniques of Seghetta et al. (2016), the P in the seaweed biomass is entirely transferred to the
165 liquid fertilizer fraction. Consequently, 100% of the P input to the extraction process follows
166 the liquid fertilizer fraction (F0,6d) while 0% ends up in the SWPC commodity (F6,7). The
167 input analysis reveals that 30.4 kg of total P input is required to produce 1 t of SPC. In
168 comparison, the total P input to SWPC is slightly lower, with a requirement of 25.05 kg for
169 each 2 t SWPC produced. The classification of P input sources reveals significant differences
170 (Fig. 8 and 9). 85% of the P input to the SPC system come in form of mineral P in fertilizer
171 and 15% is captured from naturally occurring sources. The distribution is inverted in the
172 SWPC system. Out of the total input, 99.97% and 0.03% come respectively from naturally
173 occurring and mineral sources.

174 < insert Fig8 here >

175 Fig. 8: Origin of the P flowing in the SPC system (kg)

176 < insert Fig9 here >

177 Fig. 9: Origin of the P flowing in the SWPC system (kg)

178 The SPC outflow analysis shows that each ton of SPC produced generate the emission of
179 15.46 kg (50.78%) of P to soil and water, while 14.99 kg (49.22%) is transferred to
180 anthroposphere systems (Fig. 10). The largest contributors of P transfer to the anthroposphere
181 are the crop residues (F0,3a) and the SPC fraction (F6,0d), while those generating the most
182 substantial emissions to the environment are P fixation in soil (F1,0b) and P drained by water
183 (F1,0a). For each 2 t produced in the SWPC system, 25.04 kg (99.97%) P is transferred to the
184 anthroposphere while only 0.0071 kg (0.03%) is emitted to soil and water. The only
185 significant outflow is the liquid fertilizer fraction (F6,0c) which transfers the phosphorus back
186 to the anthroposphere.

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< insert Fig10 here >

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Fig. 10: Initial fate of phosphorus outflow in the SPC system (kg)

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< insert Fig11 here >

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Fig. 11: Initial fate of phosphorus outflow in the SWPC system (kg)

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191 **4. Discussion**

192 **4.1. Implications of the primary energy consumptions**

193 4.1.1. Energy sources and production

194 For similar crude protein content, producing Norwegian SWPC requires 11.68 times more
195 primary energy than producing and importing Brazilian SPC to Norway. This considerable
196 difference in CPED could prove to be a limitation for the SWPC commodity. Larger primary
197 energy demand in a system often leads to greater global warming potential and higher
198 production costs (Sorrell, 2015). It is critical to analyze the nature of the energy mix and
199 energy production to measure the environmental impacts associated with primary energy use.
200 With current technology, the fossil-fuel requirements of the SPC and SWPC systems are
201 approximately equivalent (12,179 and 14,661 MJ respectively) and come in form of diesel,
202 heavy oil, and natural gas. This means that similar environmental impacts can be expected
203 from these inputs. However, the large quantity of electricity required for drying the seaweed
204 biomass in Norway could generate relatively little environmental impacts. The Norwegian
205 electricity mix can be supplied by nearly 100% renewable hydropower generating overall low
206 environmental burden (Itten et al., 2012). The MFA/SFA methodology is not adapted to
207 compare energy productions since it focuses on the foreground system. A comparative LCA
208 could take this analysis further and investigate the sensitivity of each system to different
209 energy mixes and their contributions to the overall environmental impacts.

210 4.1.2. Seaweed preservation

211 Seaweed is highly sensitive to microbial activity due to its high water content (85%) and must
212 be preserved shortly after harvest. Drying is an efficient way to stabilize the biomass and is a
213 conventional method to reduce weight during transportation (Keshani et al., 2010).
214 Nevertheless, current drying methods available in Norway are energy intensive and remain a
215 significant bottleneck for the SWPC system. On the other hand, these results demonstrate a
216 massive system-wide improvement potential if the preservation step can be improved. For
217 example, ensiling the macroalgae biomass is a promising alternative to drying. The ensiling
218 process typically utilizes acids to lower the pH of a fodder crop below 5, either with or
219 without a lactic acid bacterial inoculant (Herrmann et al., 2015). However, large-scale
220 ensiling processes introduce food safety concerns and may lead to new infrastructure
221 requirements to accommodate large volumes of raw material with much higher water content.
222 The cost-benefit of replacing drying with fermentation will require a life cycle analysis to sort
223 out the trade-offs between these two preservations methods.

224 Optimizing the drying process by utilizing the waste heat produced by Norwegian industry is
225 another option. In this paper, a waste incineration heat and power plant is used as a case
226 study. This facility located in Ålesund on the west coast of Norway and generates 22.5 GWh
227 of surplus energy mainly during the summer months of June and July (Tafjord, K.A., Tafjord
228 AS, Pers. Com., December 22nd, 2016). Macroalgae biomass is typically harvested in Norway
229 between April and May. June overlaps slightly with harvesting times, but in most areas, it is
230 late with respect to biofouling, which reduces the quality of the biomass (Stévant et al., 2017).
231 One option is to harvest late and utilize the waste heat from waste incineration plants,
232 sacrificing some quality for efficiency. If this option is applied, producing SWPC will then
233 require 2.3 times more primary energy than producing SPC instead of the 11.68 original
234 factor. An alternative scenario is to ensile the biomass during peak harvesting times and dry
235 the fermented material when waste heat is primarily available.

236 4.1.3. Selection and domestication

237 A multitude of factors influences the primary energy demand of each system. In this study,
238 maturity and scale had a real impact on the outcome results. The SPC value chain has been
239 optimized over decades. Selective breeding of soy varieties increased protein content and
240 yields (Koester et al., 2014). Over the last 20 years, the Brazilian government has created
241 ideal conditions for improving the capacity of SPC production processes and supply chain
242 organization (Goldsmith, 2008). The SWPC system does not benefit from a similar industrial
243 maturity. The seaweed cultivation industry has only recently selected species for
244 domestication, and is currently working on optimizing cultivation processes; transformation to
245 feed and food products has yet to be developed at an industrial scale (Skjermo et al., 2014).

246 **4.2. Implications of the Phosphorus demand**

247 4.2.1. Intensive agriculture

248 Brazilian soybeans are cultivated using intensive mono-agricultural methods. The inefficiency
249 of the soil preparation process is one of the most significant P management issues in the SPC
250 system. The MFA/SFA shows that 50.9% of the P applied for soil enrichment is not
251 transferred to *Glycine max* in the year of harvest. Instead, this P is bound to soils (F1,0b) and
252 partly drained by leaching, erosion, and surface run-off (F1,0a) (Fig. 6). Assuming continuity
253 in cultivation methods, and stable production yields, this means that farmers are overloading
254 soils with P year after year (Li et al., 2015). The high rainfall in these regions (De Freitas and
255 Landers, 2014) provides the right conditions for transport of excess P from the fields to fresh
256 and marine water bodies. For each ton of SPC produced, 84.68% of the P input comes directly

257 from rock phosphate sources, primarily from China, the United-States, and the northern
258 Sahara. Input of P through manure (F0,1b) is marginal, representing only 0.64% of the
259 cumulative P input to process 1 (Fig. 6). All P sources are not equal. Mineral fertilizers are
260 primary sources of P; they are non-renewable stocks that cannot be regenerated. Although
261 high doses of mineral fertilizer increase crops yield, the over-concentration of P in
262 agricultural soils is the single largest P loss occurring throughout the SPC system (Fig. 6). It is
263 urgent to optimize soil enrichment processes and develop alternatives to intensive
264 monocultures to mitigate this threat. Research shows that it is possible to recycle primary P
265 sources through careful management of secondary P rich co-products and wastes (Hamilton et
266 al., 2015b). Recent Brazilian research suggests that local secondary P sources could cover up
267 to 20% of the P demand of the country by 2050 (Withers et al., 2018). This means that
268 ambitious actions are needed at the policy level to incentivize the use of manure, crop
269 residues, and a new generation of bio-fertilizers.

270 4.2.2. P management performances

271 The total P consumption of the SPC system is equal to 30.4 kg/t, whereas the SWPC system
272 consumes 25.05 kg/2t. Comparing mineral P content, the SPC mineral P demand is 25.75 kg/t
273 while the SWPC system's consumption drops to 0.0083 kg/2t. Furthermore, Seghetta et al.
274 (2016) calculated a 95% substitution ratio for the seaweed fertilizer compared to mineral
275 fertilizer. In other words, the 25.05 kg of P (F0,6c) embedded in the seaweed fertilizer
276 fraction could theoretically substitute up to 23.8 kg of mineral P. Capturing P from the marine
277 environment for growth, and recycling it back to the anthroposphere in the form of a liquid
278 biofertilizer has clear advantages compared to relying on fossil P reserves from mining
279 operations. The potential of recycling the P stocked in the oceans to the anthroposphere is one
280 of the most important findings of this paper and deserves more attention. A fair comparison
281 between ocean-based P and mineral P should include a full assessment of products and by-
282 products of the two systems. Furthermore, Seghetta et al., (2016) assumes that 100% of the P
283 follow the liquid fertilizer fraction. If confirmed, this means that SWPC would be deficient in
284 P, a mineral required by salmon for optimal growth and naturally present in SPC (9.43 kg/t).
285 In this scenario, fish farmers would have to add mineral P to compensate this deficiency.
286 Analyzing the effect of different co-product environmental allocations and transfer ratios of P
287 to the SWPC commodity are outside the scope of this study and should be addressed in future
288 research.

289 **4.3. Feasibility aspects**

1 290 Cultivation area, available technology, and scale are other important considerations for
2
3 291 assessing the feasibility of substituting SPC with ocean-based proteins. Replacing 10% of
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5 292 Norwegian SPC imports would require 72,443 t of SWPC, which corresponds to 1,362,436 t
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7 293 of *S. latissima* wet-weight. With current production technology and yields (60 t/ha), this
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9 294 would require approximately 227 km² dedicated to macroalgae cultivation, in addition to the
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11 295 hatchery facilities onshore. If we compare this number to the 1,970 km² of land used for 10%
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13 296 of SPC production, SWPC requires only 11.5% of the equivalent land area at sea. Such
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15 297 cultivation efficiency could contribute to reducing the enormous pressure on terrestrial
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17 298 croplands (FAO, 2011) without occupying large areas in the marine space. Despite some
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19 299 potential environmental advantages, economic sustainability will be a key determinant of
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21 300 success for any innovative technologies, including the development of an SWPC industry in
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23 301 Norway. The small scale of production, high labor costs, and substantial primary energy
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25 302 demand are factors hindering SWPC from competing with SPC on price under current market
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27 303 conditions. If SWPC is to compete with SPC in the foreseeable future, the cost of production
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29 304 must be drastically reduced through process innovation and optimization.

29 **4.4. Uncertainty and limitation**

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31 306 Mass-balance verification is used to measure the level of data coherence in the system. This
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33 307 verification show that the SPC model is balance consistent, except for the soil preparation
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35 308 process, which displays a deficit of -0.0438 kg of P. This imbalance represents 0.14% of the
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37 309 process inputs in absolute value and is well within the frame of inherent data uncertainty. The
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39 310 SWPC system is mass-balanced, indicating good data convergence.

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41 311 MFA/SFA models are based on parameters from a wide variety of data sources. Each
42
43 312 parameter contains uncertainty that adds up to an overall level of uncertainty in the final
44
45 313 model. Evaluating uncertainty is critical to understanding the integrity of the system and
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47 314 results of system analysis. Ideally, a quantitative uncertainty analysis should have been
48
49 315 performed in this study, but the extensive use of industry data with unknown uncertainty
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51 316 hampered this effort. However, inferences about model uncertainty can be made based on
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53 317 high impact flows. For instance, parameters such as the production methods, cultivation
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55 318 yields, and mineral fertilizer inputs are assumed to have a strong influence on the SPC
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57 319 system's results. Similarly, in the SWPC system, results are expected to be highly sensitive to
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59 320 cultivation yield, seaweed dry matter content, and biorefinery extraction ratios. In the SPC
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61 321 system, processes 1 to 4 were constructed with a high level of detail due to the good quality of
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322 Da Silva's dataset (Da Silva et al., 2010). Processes 5 and 6 include numerous assumptions
323 and a broad diversity of data sources and are assumed to contain a higher degree of
324 uncertainty. The SWPC system suffers from similar limitations. The youth of the seaweed
325 industry is a challenge to the modeling. The whole cultivation process is based on the
326 production of a single company. Although Hortimare is a leading actor in European
327 macroalgae cultivation and uses industry-standard technology, this is perhaps the most
328 significant limitation of this model.

329 Adjusting the two systems for protein equivalency is a controversial step and uncommon in
330 MFA. A major limitation to the integrity of this technique is the quality of the protein. SPC
331 from *Glycine max* is a highly digestible feed ingredient bred to limit anti-nutritional factors
332 that could affect fish growth (Storebakken et al., 1998). SWPC has not been tested in fish
333 nutrition, so very little can be said about the suitability of this protein, despite being equal to
334 SPC in gross protein output once the systems are adjusted. Other important factors to consider
335 is that 2 tons of 31% protein will mean that twice the amount of raw material will have to
336 enter the feed mill. Unless the SWPC has a nutritional advantage over SPC, the added volume
337 will create unwanted adjustments for manufacturer in logistics, storage, transport, and feed
338 formulation to replace the ubiquitous SPC. Therefore, before one can truly begin to assess the
339 viability of SWPC replacing SPC at the system's level, extensive studies must be performed
340 to test the suitability of the raw material as a feed ingredient in finfish nutrition. Finally,
341 biorefinery processes should focus on developing an SWPC product with similar protein
342 content to SPC to lower the cost of adoption for feed producers.

5. Conclusion

345 This study is motivated by recent efforts highlighting the Norwegian aquaculture feed
346 industry's reliance on imported agricultural commodities generating significant environmental
347 impacts in other countries. Brazilian SPC is one of the most common protein-rich ingredients
348 used in Norwegian compound feeds and is produced with high and inefficient use of fossil P
349 fertilizers. With current technology, substituting SPC by SWPC is an environmental trade-off.
350 Such a substitution would largely increase the primary energy consumption of protein-rich
351 feed ingredients, but would likely reduce eutrophication, mineral P depletion, as well as land
352 and freshwater use. P management efficiency in food and feed production systems is vital for
353 current and future food security. It is also where lays the sustainable advantage of seaweed

354 feedstock compared to land-based crops. This study was performed at an advantageous time
1 355 to identify potential system enhancements in the emerging Norwegian macroalgae-based
2 356 bioeconomy. The 11.68 times high primary energy of the SWPC system vs. the SPC system is
3 357 mainly a result of the drying process required to remove water from the macroalgae biomass.
4 358 In addition to the benefits of upscaling and optimizing the production, sizeable primary
5 359 energy demand reduction can be achieved utilizing secondary energy and/or ensiling. Several
6 360 potential drawbacks and unresolved issues impede the adoption of SWPC by the aquafeed
7 361 industry. SPC is a well-established ingredient in animal nutrition and became over the years a
8 362 standard ingredient in many aquafeed. SWPC is untested for nutritional suitability,
9 363 digestibility, and palatability in animal nutrition and is currently only available at 31% protein
10 364 concentration, about half of SPC's standard 62%. Further research is also required to analyze
11 365 in-depth the allocation of each system's co-products. In this perspective, a comparative LCA
12 366 would allow the influence of indirect and direct emissions on a broader range of
13 367 environmental impacts to be included in the analysis. Such a study would be a natural
14 368 extension of this work.
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564 Table 1 - Flow description of the SPC system

Flows	Equations & sources
Process 1 - Soil preparation	
F0,1a - [P] Mineral fertilizers	Mineral fertilizer P ₂ O ₅ content PT _{1,3,5,6} ¹ × corresponding PT/region PR ₁ ¹ × P ₂ O ₅ P content ¹
F0,1b - [P] Manure	Manure P ₂ O ₅ content PT _{2,4} ¹ × corresponding PT/region PR ₁ ¹ × P ₂ O ₅ P content ¹
F0,1c - [P] Crop residues	Leaves-stems-pods P ₂ O ₅ uptake TP _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × P ₂ O ₅ P content ¹
F0,1d - Diesel, maintenance	(Diesel ploughing & subsoiling PT _{1,2,5} + diesel tilling PT _{3,4,5} + diesel dethatching PT _{3,4,5} + diesel fertilizer application PT _{1,3,5,6} + diesel manure application PT _{2,4}) × corresponding PT/region PR ₁ ¹
F0,1e - Diesel, transport inputs	Load-distance ingredient PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × lorry diesel consumption ²
F1,0a - [P] Drained by water	PO ₄ to water PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × PO ₄ P content ¹
F1,0b - [P] Fixation in soil	(P ₂ O ₅ to soil PT _{1,2,3,4,5,6} – PO ₄ to underground water) × corresponding PT/region PR ₁ ¹ × corresponding P ₂ O ₅ / PO ₄ P content ¹
F1,2 - [P] Net primary production	P in leaves-stems-pods ¹ + P in beans ¹ – P in seeds ¹
Process 2 - Seedling & growth	
F0,2a - [P] Seeds	Seeds input PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × seed P content ¹
F0,2b - [P] Biocides	(Glyphosate input PT _{1,2,5} + methamidophos input PT _{1,2,3,4,5,6}) × corresponding PT/region PR ₁ ¹ × corresponding glyphosate / methamidophos P content ¹
F0,2c - Diesel, seedling	Diesel seedling PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹
F0,2d - Diesel, biocides	Diesel biocides applications PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹
F2,0a - [P] Biocides dispersion	(Glyphosate input PT _{1,2,5} + methamidophos input PT _{1,2,3,4,5,6}) × corresponding PT/region PR ₁ ¹ × corresponding glyphosate / methamidophos P content ¹
F2,3 - [P] Soy plants	P in leaves-stems-pods ¹ + P in beans ¹
Process 3 - Harvest	
F0,3a - Diesel, harvesting	Diesel harvesting PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹
F0,3b - Diesel, transport to farm	Diesel transport to farm PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹
F0,3c - Diesel, transport to storage	Load-distance soybeans PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × lorry diesel consumption ²
F3,0a - [P] Crop residues	Leaves-stems-pods P ₂ O ₅ uptake TP _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × P ₂ O ₅ P content ¹
F3,0b - [P] Seeds, next harvest	Seeds output PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × seed P content ¹
F3,4 - [P] Soybean, 18% water	(P ₂ O ₅ uptake beans PT _{1,2,3,4,5,6} × corresponding PT/region PR ₁ ¹ × P ₂ O ₅ P content ¹) – seeds P content ¹
Process 4 - Drying & storage	
F0,4 - Wood chips, drying	Woodchips energy for drying ³ + electricity energy cleaning & storage ⁴
F4,0 - [P] Soybean, 13% water	P ₂ O ₅ uptake beans PT _{1,2,3,4,5,6} ¹ × corresponding PT/region PR ₁ ¹ × P ₂ O ₅ P content ¹
Process 5 – Extraction	
F0,5a - Diesel, transport to factory	(Load-distance road × lorry diesel consumption) ^{3,2} + (load-distance railway × freight train diesel consumption) ^{3,4} + (load-distance waterway × barge freight diesel consumption) ^{3,4}
F0,5b - Energy, extraction	Diesel-energy input ³ + electricity-energy input ⁴ + natural gas-energy input ³
F5,0a - [P] Soybean, hulls	Soybean hulls output ⁵ × soybean hulls P proportion ⁵
F5,0b - [P] Soybean, crude oil	Soybean crude oil output ⁶ × soybean crude oil P proportion ⁶
F5,0c - [P] Soybean, molasses	Soybean molasses output ⁷ × soybean molasses P proportion ⁷
F5,6 - [P] SPC, 8% water	SPC output ⁸ × SPC P proportion ⁸
Process 6 - Import to Norway	
F0,6a - Diesel, transport to port	((Load-distance road Sorriso to Porto de Santos/Porto de Imbituba ^{9,10} × corresponding port UR ⁹ × Caramuru MS) + (load-distance road Araucária to Porto de Paranaguá ^{11,10} × Imcopa MS) × lorry diesel consumption ²) + (load-distance railway Araguari to Porto de Vitória ^{12,10} × Selecta MS × freight train diesel consumption ⁴)
F0,6b - Diesel, transport Rotterdam	((Load-distance shipping Porto de Santos/Porto de Imbituba to R ^{9,13} × corresponding port UR ⁹ × Caramuru MS) + (load-distance shipping Porto de Paranaguá to R ^{11,13} × Imcopa MS) + (load-distance shipping Porto de Vitória to R ^{12,13} × Selecta MS)) × freight shipping heavy fuel oil consumption ⁴
F0,6c - Diesel, transport to Norway	((Load-distance shipping R to Myre/Karmøy ^{14,13} × corresponding factories UR ¹⁴ × Biomar MS ¹⁵) + (load-distance shipping R to Florø/Halsa/Bergneset ^{16,13} × corresponding factories UR ¹⁶ × Ewos MS ¹⁵) + (load-distance shipping R to Stavanger/Averøy/Stokmarknes ^{17,13} × corresponding factories UR ¹⁷ × Skretting MS ¹⁵)) × freight shipping diesel consumption ¹⁸
F6,0d - [P] SPC, 8% water	SP output ⁸ × SPC P proportion ⁸

565 **Abbreviations:** MS = Market Share; PT = Production Types; P = Phosphorus; PR = Production Ratios; R = Rotterdam; UR = Use
 566 Ratios.

567 **Sources:** ¹(Da Silva et al., 2010); ²(Spielmann and Scholz, 2005); ³(Hognes et al., 2014); ⁴(Spielmann et al., 2007); ⁵(Barbosa et al.,
 568 2008); ⁶(Knoll and Life, 2007); ⁷(Hall et al., 2005); ⁸(Endres, 2001); ⁹(Caramuru, Pers. Com., November 15th, 2016); ¹⁰(Google
 569 Maps, 2016); ¹¹(Imcopa, Pers. Com., November 14th, 2016); ¹²(Sugui, P.R., Selecta, Pers. Com., November 14th, 2016); ¹³(SeaRates,
 570 2016); ¹⁴(Skansen, T., Biomar, Pers. Com., November 21st, 2016); ¹⁵(Rana et al., 2009); ¹⁶(Ewos, Pers. Com., November 22th, 2016);
 571 ¹⁷(Skretting, Pers. Com., November 21st, 2016); ¹⁸(Gabi Software, 2016).

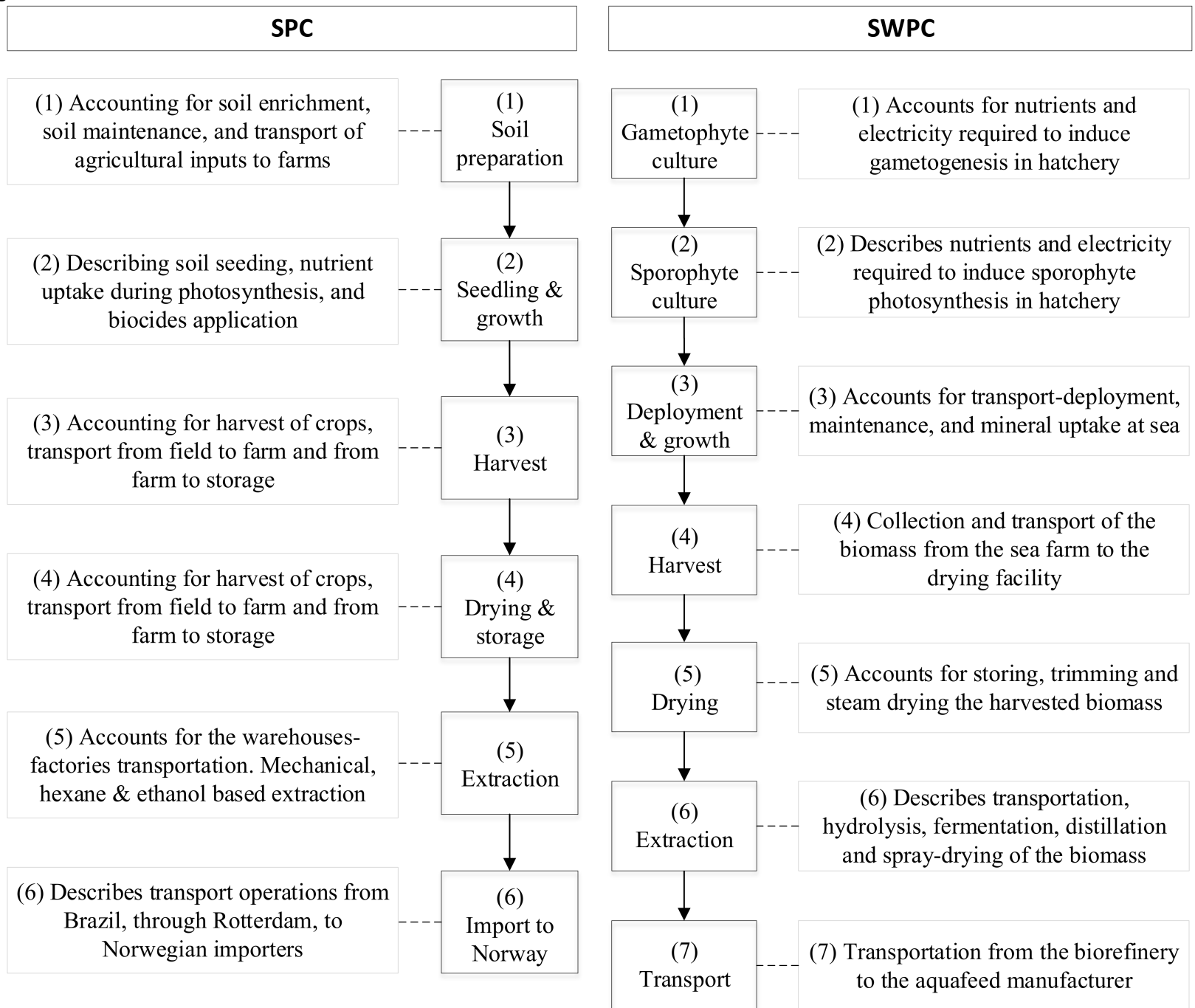
572 Table 2 - Flow description of the SWPC system

Flow	Equations & sources
Process 1 - Gametophyte culture	
F0,1a - [P] Gametophyte, year -1	Gametophyte biomass inoculated ^{1,2,3} × <i>S. latissima</i> gametophyte P content
F0,1b - [P] Culture nutrients	F/2 medium NaH ₂ PO ₄ ·2H ₂ O concentration ⁴ × SW culture volume ⁵ × NaH ₂ PO ₄ ·2H ₂ O P content
F0,1c - [P] Seawater	SW culture mass ⁵ × SW P content, July/August ⁵
F0,1d - Electricity, hatchery	(White light power × HU × quantity) ³ + (red light power × HU × quantity) ³ + (air conditioning power × HU × quantity) ³ + (aeration pump power × HU × quantity) ³ + (autoclave power × HU × quantity) ³
F1,0a - [P] Used enriched seawater	((SW culture mass × SW P content, July/August) ^{3,5} + (F/2 medium NaH ₂ PO ₄ ·2H ₂ O concentration × SW culture volume × NaH ₂ PO ₄ ·2H ₂ O P content) ^{3,4}) × gametophyte P non-uptake fraction
F1,0b - [P] Gametophyte, year +1	Gametophyte biomass inoculated ³ × <i>S. latissima</i> gametophyte P content
F1,0c - [P] Gametophyte, losses	NPP gametophyte biomass P content ^{3,4,5} × gametophyte loss ratio
F1,2 - [P] Gametophyte biomass	NPP gametophyte biomass P content ^{3,4,5} × gametophyte settlement ratio
Process 2 - Sporophyte culture	
F0,2a - Electricity, hatchery	(White light power × HU × quantity) ³ + (aeration pump power × HU × quantity) ³ + (UV treatment power × HU × quantity) ³ + (climatization power × HU × quantity) ³ + (filtration system power × HU × quantity) ³
F0,2b - [P] Seawater	F/2 medium NaH ₂ PO ₄ ·2H ₂ O concentration ⁴ × SW tank volume ⁵ × NaH ₂ PO ₄ ·2H ₂ O P content
F0,2c - [P] Culture nutrients	F/2 medium nutrient concentration ⁴ × SW tank volume ⁵ × nutrients inputs over time ³
F2,0b - [P] Used enriched seawater	((SW tank mass × SW P content, September) ^{3,5} + (F/2 medium NaH ₂ PO ₄ ·2H ₂ O concentration × SW tank volume × NaH ₂ PO ₄ ·2H ₂ O P content) ^{3,4}) × sporophyte P non-uptake fraction
F2,3 - [P] Sporophyte biomass	Quantity of P in gametophyte biomass ^{3,4,6,7} + NPP sporophyte biomass P content ^{3,4,5}
Process 3 - Deployment & growth	
F0,3a - Fuels, transport to farm	((Distance H-H × RM × FT diesel consumption) ³ + (distance H-F × RM × SB diesel consumption) ³ + (distance H-F × RM × MB petrol consumption) × number of trips) ³ + (deployment distance × MB petrol consumption) ³
F0,3b - Fuels, maintenance	((Distance H-H × RM × FT diesel consumption) ³ + ((distance H-F × RM) + maintenance distance) × MB petrol consumption) ³ × number of trips ³
F0,3c - [P] Uptake, open seawater	Quantity of P in seaweed biomass ^{3,8,9,10} – quantity of P in sporophyte biomass ^{3,4,5,6,7}
F3,4 - [P] Seaweed biomass	Quantity of seaweed biomass ³ × <i>S. latissima</i> DM content ⁸ × <i>S. latissima</i> P content ¹⁰
Process 4 - Harvest	
F0,4 - Fuels, transportation	Load-distance, pontoon deployment × RM × NabCat diesel consumption) ^{3,11} + ((distance H-H × RM × FT diesel consumption) ³ + ((distance H-F × RM + maneuvering distance) × MB petrol consumption) ³ + (harvest hours × generator diesel consumption) ³ + (load-distance F-H × RM × NabCat diesel consumption) ^{3,11} + (load-distance H-DF × RM × refrigerated lorry diesel consumption) ^{3,12} × harvest days
F4,5 - [P] Seaweed, 85% H ₂ O	Quantity of seaweed biomass ³ × <i>S. latissima</i> DM content ⁸ × <i>S. latissima</i> P content ¹⁰
Process 5 - Drying	
F0,5a - Steam heat, drying	Convective dryer steam requirement ¹³ × quantity of seaweed biomass ³ × seaweed shrinkage ratio ⁸
F0,5b - Electricity, drying facility	(Transverse slicer power × HU × quantity) ¹⁴ + (convective dryer power × HU × quantity) ¹⁵ + (climatization power × HU × quantity) ¹⁵
F5,6 - [P] Seaweed, 20% H ₂ O	Quantity of seaweed, 85% H ₂ O ³ × <i>S. latissima</i> DM content ⁸ × <i>S. latissima</i> P content ¹⁰
Process 6 - Extraction	
F0,6a - Diesel, transportation	Load-distance DF-BR × lorry diesel consumption ¹⁶
F0,6b - Heat, extraction	Heat-energy hydrolysis & fermentation ⁸ + heat-energy distillation ⁸
F0,6c - Electricity, extraction	Energy feedstock handling ⁸ + energy enzyme production ⁸ + energy storages & utilities ⁸
F0,6d - [P] Liquid fertilizer	Seaweed, 20% H ₂ O P content ^{3,8,10} × liquid fertilizer P TC ⁸
F6,7 - [P] SWPC	Seaweed, 20% H ₂ O P content ^{3,8,10} × SWPC P TC ⁸
Process 7 - Transportation	
F0,7 - Diesel, transportation	(Load-distance BR-H × lorry diesel consumption) ¹⁶ + (load-distance H-FFF × ship diesel consumption) ¹⁷
F7,0b - [P] SWPC	Seaweed, 20% H ₂ O P content ^{3,8,10} × SWPC P TC ⁸

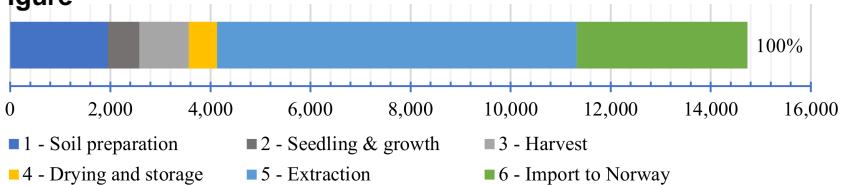
573 Abbreviation: SW = Sea Water; HU = Hours Used; NPP = Net Primary Production; H-H = Hatchery-Harbor; H-F = Harbor-Farm;
 574 RM = Roundtrip Multiplier; SB = “Snekke” Boat; MB = Maneuvering Boat; DM = Dry Matter; F-H = Farm-Harbor; H-DF =
 575 Harbor-Drying Facility; DF-BR = Drying Facility-BioRefinery; TC = Transfer Coefficient; BR-H = BioRefinery-Harbor; H-FFF =
 576 Harbor-Fish Feed Factory.

577 Sources: ¹(Zhang et al., 2007); ²(Xu et al., 2009); ³(Van Den Heuvel, F., Hortimare, Pers. Com., December 8th, 2016); ⁴(Guillard and
 578 Rytter, 1962); ⁵(Moy et al., 2016); ⁶(Skjermo, J., Sintef, Pers. Com., December 16th, 2016); ⁷(Hornstje, 2014); ⁸(Seghetta et al., 2016);
 579 ⁹(Vilg et al., 2015); ¹⁰(Manns et al., 2014); ¹¹(Hansvik, T., Moen Marin, Pers. Com., December 22th, 2016); ¹²(Keller, 2010);
 580 ¹³(Sandvik Process Systems, 2016); ¹⁴(FAM, 2016); ¹⁵(Kide, 2016); ¹⁶(Spielmann and Scholz, 2005); ¹⁷(Gabi Software, 2016).

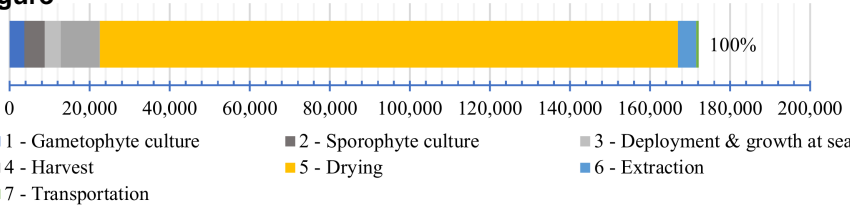
Figure



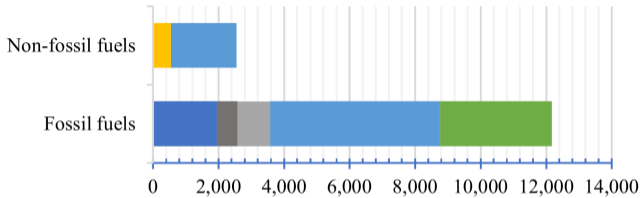
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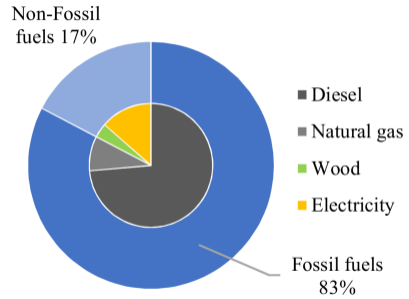
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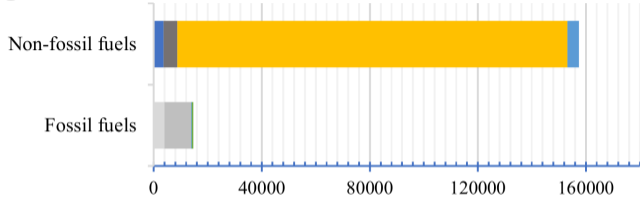
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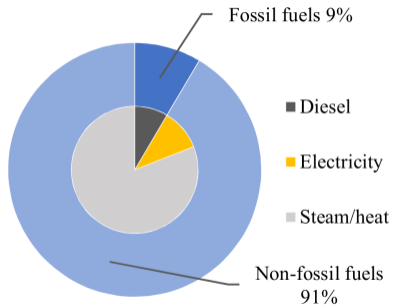
- 1 - Soil preparation
- 2 - Seedling & growth
- 3 - Harvest
- 4 - Drying and storage
- 5 - Extraction
- 6 - Import to Norway



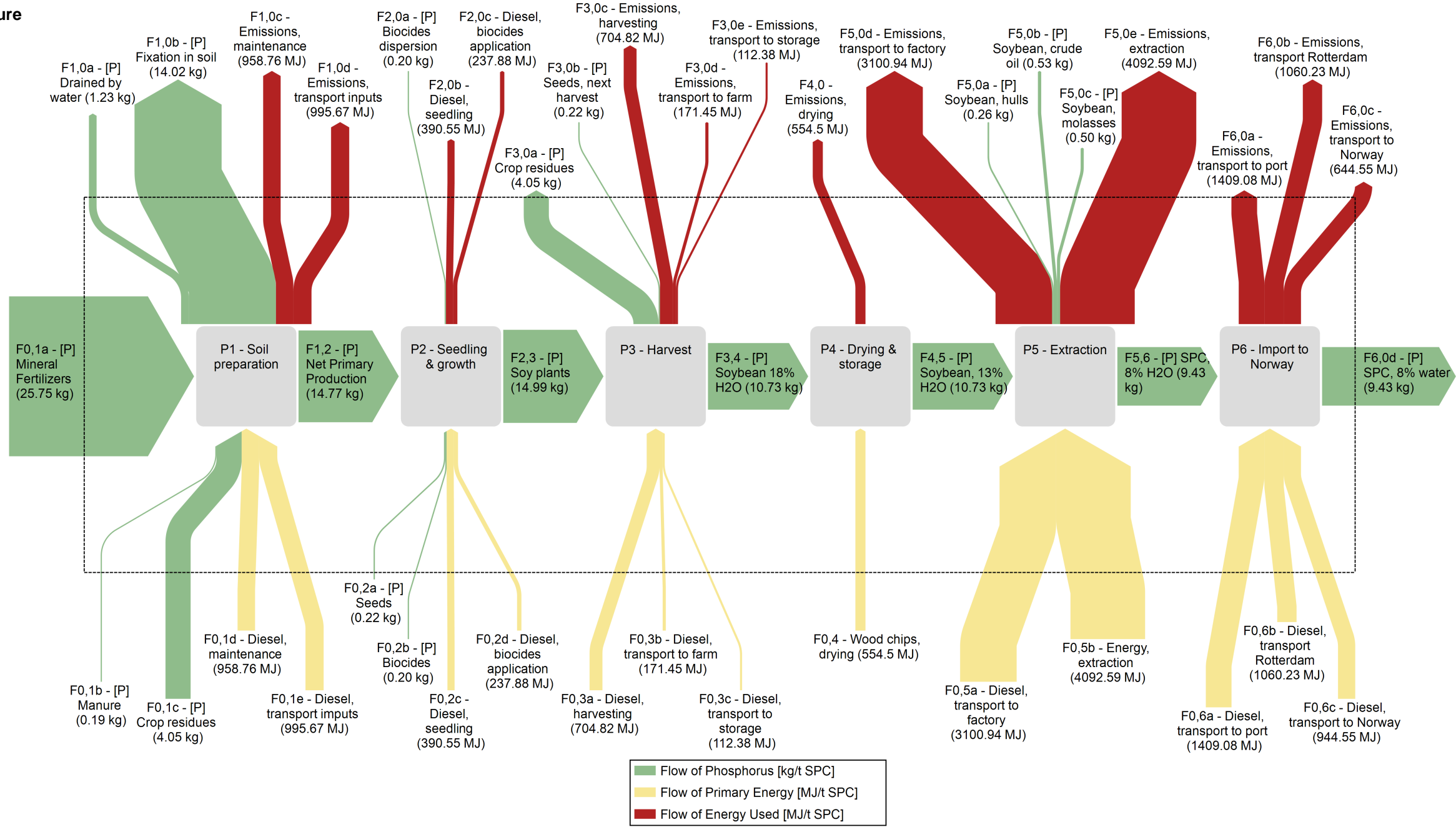
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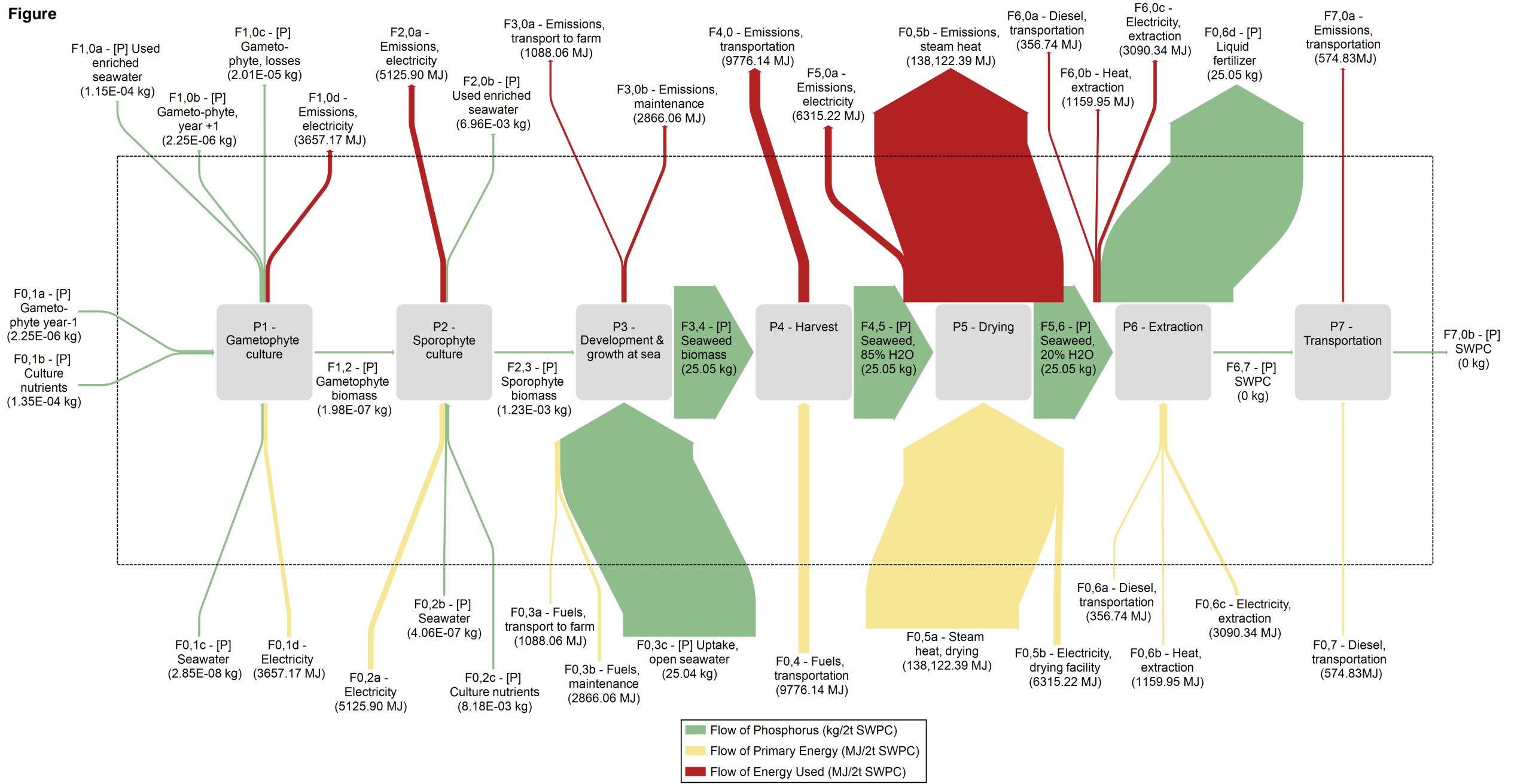
- 1 - Gametophyte culture
- 2 - Sporophyte culture
- 3 - Deployment & growth at sea
- 4 - Harvest
- 5 - Drying
- 6 - Extraction
- 7 - Transportation



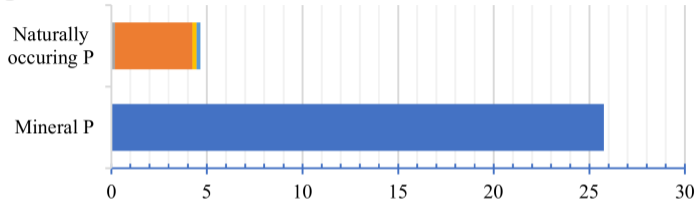
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Figure



Figure



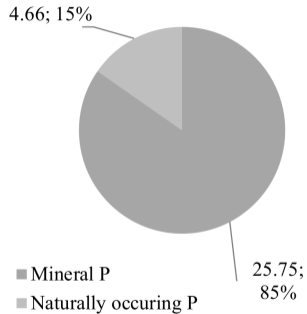
■ 0,1a - [P] Mineral fertilizers

■ 0,1c - [P] Crop residues

■ 0,2b - [P] Biocides

■ 0,1b - [P] Manure

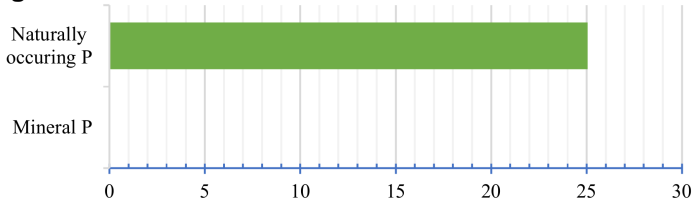
■ 0,2a - [P] Seeds



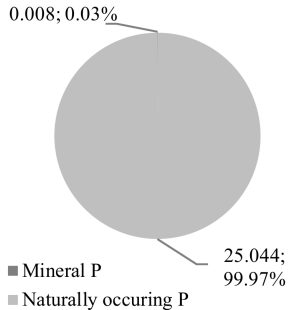
■ Mineral P

■ Naturally occurring P

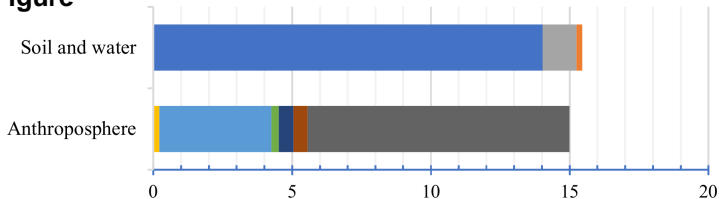
Figure



- 0,1a - [P] Gamethophyte, year-1
- 0,1b - [P] Culture nutrients
- 0,1c - [P] Seawater, sterilized
- 0,2b - [P] Seawater
- 0,2c - [P] Culture nutrients
- 0,3c - [P] Uptake, open seawater



Figure



■ 1,0a - [P] Fixation in soil

■ 2,0 - [P] Biocides dispersion

■ 3,0b - [P] Crop residues

■ 5,0b - [P] Soybean, crude oil

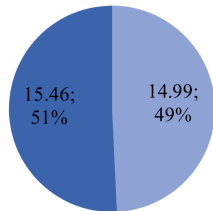
■ 6,0 - [P] SPC, 8% water

■ 1,0b - [P] Drained by water

■ 3,0a - [P] Seeds, next harvest

■ 5,0a - [P] Soybean, hulls

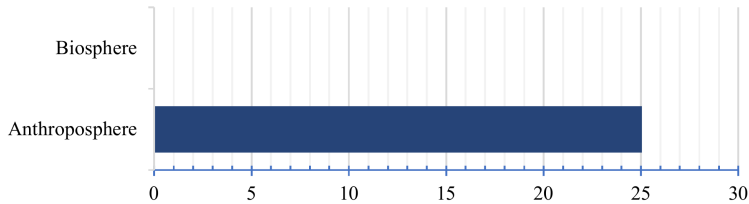
■ 5,0c - [P] Soybean, molasses



■ Anthroposphere

■ Soil and water

Figure



- 1,0a - [P] Used enriched seawater
- 1,0c - [P] Gametophyte, losses
- 6,0d - [P] Liquid fertilizer

- 1,0b - [P] Gametophyte, year+1
- 2,0b - [P] Used enriched seawater
- 7,0b - [P] SWPC

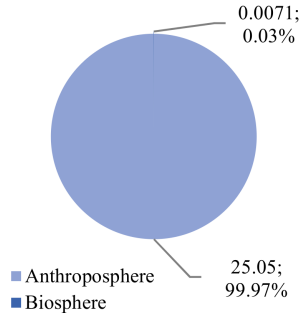


Table 3 - Description of assumptions made in the SPC system

SPC MFA/SFA assumptions description

1. Production yield is constant over time

Constant production yield allows for simplifying calculations involving crop residues and seeds inputs and outputs.

2. Soybean seeds and crop residues are direct outputs of the system from the third process

Soybean seeds and crop residues are treated as outputs of the system although they can be considered as short-term stocks. This assumption facilitates calculations.

3. 100% of the biocides are dispersed into the biosphere

Accounting for biocides settlement on crops implied complex calculation whereas it is estimated that quantities of chemical deposits on crops are neglectable.

4. Caramuru, Imcopa, and Selecta hold 100% of the Brazilian SPC market share, and weight respectively 1/3rd each

This assumption reduces the complexity of logistical modelling. It is based on Biomar supplier network (Skansen, T., Biomar, Pers. Com., November 21st, 2016).

5. All SPC imports transit through Rotterdam

The transition of the SPC cargo through Rotterdam is based on Biomar logistics (Skansen, T., Biomar, Pers. Com., November 21st, 2016). Assuming all cargo follow the same route reduces the process complexity.

6. Ewos, Biomar, and Skretting hold 100% of the Norwegian aquafeed market share

These three leading aquafeed producers are by far the main Brazilian SPC importers to Norway (Lundeberg and Grønlund, 2017).

7. All imported Brazilian SPC contains 62% protein

The SPC produced by Imcopa contain minimum 62% protein (Hognes et al., 2014). It simplifies the system to assume that all SPC imported to Norway has the same protein content.

8. 100% of the SPC imported by Norway come from Brazil

In reality, approximately 94% of the SPC imported by to Norway come from Brazil (Lundeberg and Grønlund, 2017). This assumption narrows the scope of this study on Brazilian SPC.

8. The input and output of P from crop residues flows in a closed loop and does not affect other flows of the system

The input and output of P from crop residues are not accounted for in the LCA by Da Silva et al. (2010). This set of assumptions simplifies the system without compromising the P cycle (the growing plants capture 100% of the P in crop residues from the previous harvest; this P is entirely transferred to the crop straws; at harvest, the crop straws become crop residues again, and this P fraction leave the system).

10. Drying does not affect the P content of food/feed commodities

Drying processes do not affect quantities of minerals like P. Reducing the water fraction concentrates minerals but does not affect the absolute quantity (Adepoju and Adefila, 2015).

11. The P content in process water is negligible.

It was assumed that the quantity of P following the process water produced during soybean extraction was negligible compared to the quantity in the product and co-products.

Table 4 - Description of assumptions made in the SWPC system

SWPC MFA/SFA assumptions description

1. Gametophytes and sporophytes use 15% of the F/2 medium nutrients (added nutrients + seawater nutrients)
Data scarcity was a severe limitation for modelling gametophyte and sporophyte culture. It was assumed that gametophytes and sporophytes grow in a large excess of nutrients (Van Den Heuvel, F., Hortimare, Pers. Com., December 8th, 2016; Marfaing, H., Ceva, Pers. Com., January 5th, 2017) and only use a fraction of the nutrients available.
2. All gametophyte losses occur during the settlement of gametophyte on twines
Gametophytes, sporophytes, and seaweed plants fall from the culture support as a natural part of the seaweed lifecycle. This phenomenon is not adapted to modelling.
3. The chemical composition of *S. latissima* reflects the nutrient absorption occurring at sea; Consequently, uptake calculations are based on ash content (Vilg et al., 2015).
Determining nutrient uptake from seawater under experimental conditions is outside of the scope of this study. Using published chemical composition is more adapted to this environmental assessment.
4. Hatchery production, sea farming and harvest occur near Ålesund (Norway)
This assumption is essential to integrate the cultivation and transformation sections of the supply chain. Land-based transformation cannot realistically occur in Solund, and large-scale transport of the biomass from Solund to Ålesund is not desirable from an operation standpoint. Ålesund is a major port with excellent characteristics to establish biorefineries.
5. The biomass is transported to a drying facility next to the waste incineration heat and power plant Tafjord Kraftvarme in Ålesund (Norway)
This assumption provides the possibility to use the excess heat produced by the facility during summer months.
6. The biomass is processed with a transverse slicer and a convective belt dryer
Industrial seaweed drying processes are not currently in operation in Norway. The drying process was therefore modelled using a convective belt dryer adapted to the biomass that enables the use of secondary steam heat (Nordtvedt, T., Sintef Ocean, Pers. Com., December 22nd, 2016).
7. The steam heat required for drying is produced from the Norwegian electricity mix.
In Norway, electricity is easily accessible and almost exclusively based on renewable hydropower sources (Itten et al., 2012). Electricity is, therefore, the most likely energy source used in these conditions.
8. The bio-extraction of *S. latissima* described in Seghetta et al. (2016) can be utilized in a biorefinery near Ålesund, Norway.
Industrial seaweed biorefineries are not currently available in Norway. The modelling of the extraction process is entirely based the high-resolution data from this recent biorefinery LCA study performed in Denmark (Seghetta et al., 2016).
9. The drying facility is located 20 km away from the harbour. The biorefinery is within a 30 km range from the drying facility and 20 km from the closest harbour. The closest fish feed factory is located at 100 km by boat.
The logistics system was modelled based on assumptions focusing on limiting distances between raw material landing, drying and processing.
10. 2t of SWPC provides the same functional unit as 1t of SPC.
The protein content of SWPC produced according to Seghetta et al. (2016) contains 31.34% crude protein while SPC contains a minimum of 62% (Hognes et al., 2014).
Consequently, approximately twice the amount of SWPC is necessary to obtain the same quantity of crude protein.

Adepoju, O.T., Adefila, S.A., 2015. Effects of Processing Methods on Nutrient Retention of Processed Okro (*Abelmoschus Esculentus*) Fruit. *Journal of Food Research* 4(6), 62.
<http://dx.doi.org/10.5539/jfr.v4n6p62>

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<https://doi.org/10.1016/j.jenvman.2010.04.001>

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Itten, R., Frischknecht, R., Stucki, M., Scherrer, P., Psi, I., 2012. Life cycle inventories of electricity mixes and grid. Treeze Ltd. / Zurich University of Applied Sciences.

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Vilg, J.V., Nylund, G.M., Werner, T., Qvirist, L., Mayers, J.J., Pavia, H., Undeland, I., Albers, E., 2015. Seasonal and spatial variation in biochemical composition of *Saccharina latissima* during a potential harvesting season for Western Sweden. *Botanica Marina* 58(6), 435-447.
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