

1 The influence of lipid composition, storage temperature, and modified
2 atmospheric gas combinations on the solubility of CO₂ in a seafood
3 model product

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16 **Abstract**

17 The demand for tasty, convenient, fresh seafood products is continually increasing. This stresses the
18 need for processing methods that can prolong the otherwise short shelf life of seafood. A well-studied
19 method is the use of modified atmosphere packing. However, research into the use of modified
20 atmosphere packaging for seafood with varying lipid composition is limited. Thus, in this experiment
21 the effect of lipid profile, storage temperature, and the gas composition of the modified atmosphere
22 on the solubility of CO₂ in a seafood model product was investigated. The temperature dependent
23 Henry's constants for the various compositions showed that the physical state of the lipids clearly
24 influenced the solubility of CO₂ in the model products, with liquid fat leading to a similar solubility of
25 CO₂ as water, while CO₂ only being minimally dissolved in solid fats.

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28 **Keywords**

29 Modified atmosphere packaging; seafood model product; lipid composition; storage temperature; gas
30 composition

31

32 1 Introduction

33 Recent socio-economic development has led to an increase in time pressure brought about by work
34 and pastime activities as well as increasing amounts of single person and/or small households
35 (Speranza et al., 2009). Extensive campaigning has increased consumers awareness of the benefits of
36 fish and seafood, however many feel a lack of abilities and experience with preparing seafood. This has
37 tremendously increased the demand for convenient, tasty meal products based on fresh fish (Hansen
38 et al., 2015; Mendes and Gonçalves, 2008). Fresh seafood has a limited shelf life as a result of multiple
39 factors often specific to these particular foods, including high post mortem pH, presence of large
40 amounts of unsaturated fatty acids (affected by fish species), and presence of autolytic enzymes (Gram
41 and Huss, 1996; Sivertsvik et al., 2002). The nature of seafood stresses the need for improved
42 preservation methods that allow extension of shelf life. Multiple technologies are being used for this
43 purpose, and modified atmosphere packaging (MAP) in combination with refrigeration has become
44 one well-established method (Lambert et al., 1991). Several studies have found MAP to extend shelf
45 life for several days compared to air storage depending on species and temperature (Powell and
46 Tamplin, 2012; Sivertsvik et al., 2003; Speranza et al., 2009; Torrieri et al., 2006; Tsironi and Taukis,
47 2010; Özogul et al., 2004). The spoilage of fish begins as soon as the fish dies and is ascribed to a series
48 of reactions where degradation is caused by bacteria (Speranza *et al.*, 2009).

49 MAP often uses a mixture of oxygen (O₂), nitrogen (N₂), and carbon dioxide (CO₂), and the
50 prolongation of shelf life is often ascribed to the bacteriostatic effect of CO₂ (Genigeorgis, 1985). A
51 certain amount of CO₂ has to be dissolved into the food in order to inhibit bacterial growth (Gill and
52 Penney, 1988), and it has been found that the inhibition obtained is proportional to the concentration
53 of dissolved CO₂ (Devlieghere et al., 1998a, b). CO₂ is generally highly soluble in both muscle and fatty
54 tissues and even more so in pure water (Gill, 1988). Several factors will however influence the uptake;
55 including pH, lipid content, lipid type (Gill, 1988; Jakobsen and Bertelsen, 2004), salt content (Rumpf
56 et al., 1994), amount of initial CO₂ in the gas mixture (Devlieghere *et al.*, 1998a), and water content
57 (Sivertsvik et al., 2004). Several studies have found that solubility of CO₂ in muscle food could be
58 estimated based on the water content alone, for instance in raw fish (Sivertsvik *et al.*, 2004), chicken
59 (Rotabakk et al., 2010), and meat (Gill, 1988). However disagreements exists as Fava and Piergiovanni
60 (1992) concluded the solubility of CO₂ in fresh meat and meat products estimated based on water
61 content alone was misleading. Probably the most important factor influencing the solubility of CO₂ is
62 temperature. This effect has been extensively studied, amongst other by Gill (1988), Mendes et al.
63 (2011), and Rotabakk (2013). Previous results generally agree that increasing temperatures will
64 decrease the solubility of CO₂ in muscle tissues, just as it is known from water (Caroll et al., 1991). The
65 relationship between temperature and solubility of CO₂ in fatty samples is not as simple. Rotabakk
66 (2013) found the solubility of CO₂ in liquid salmon oil to be similar to that in water. However, when Gill

67 (1988) examined the solubility of CO₂ in fat from lamb, beef, and pork, he found the solubility to
68 increase with increasing temperatures, to a certain point, unlike that seen in water or muscle tissue.
69 The point at which increasing temperatures led to a decrease in solubility of CO₂ was different for the
70 different fat sources. These results shows that the effect of temperature on the solubility of CO₂ in
71 fatty tissue is more complex than other samples and the mechanism is not well understood (Gill, 1988;
72 Jakobsen and Bertelsen, 2006). Besides shelf life, solubility of CO₂ also influences the risk of packages
73 collapsing (Rotabakk and Sivertsvik, 2012). Thus, understanding and manipulating the solubility of CO₂
74 in various products is important from both a packaging and shelf life point of view. This underlines the
75 fact that different foods, with different compositions have to be treated differently. Thus, in order to
76 optimize the industrial use of MAP it is essential to obtain knowledge regarding the specific product
77 and processing of interest in relation to the solubility of CO₂.

78 Even though solubility of CO₂ in various products is well studied, comparison between studies
79 are often difficult. Furthermore, investigation of the solubility of CO₂ in seafood products with varying
80 lipid composition is limited. The aim of this study is thus to expand the knowledge of the solubility of
81 CO₂ in seafood by studying the effect of lipid phase composition of a fish mince model product,
82 temperature, and initial gas mix.

83 2 Materials and methods

84 A three-factor storage experiment was conducted, the factors being lipid composition (mix of stearic
85 acid, oleic acid and an **eicosapentaenoic acid (EPA)/docosahexaenoic acid (DHA)** mix), storage
86 temperature (0°, 8°, and 20°C), and packaging gas CO₂ concentration (35, 50, and 70%, balanced with
87 N₂).

88 2.1 Production of fish model product

89 Frozen mince of silver smelt (*Argentina silus*) were purchased from Norwegian Seafood Company. The
90 fish mince had a water content of 69.8±0.5% and lipid content of 1.2±0.1%. The lipid phase was
91 primarily made up of saturated- and monounsaturated fatty acids (6% C14:0, 37% C16:0, 6% C18:0,
92 20% C18:1, 12% C20:1, 15% C22:1). The fish mince was thawed at 4°C for 24 hours prior to being mixed
93 in a bowl chopper (Blixer 6, Robot Coupe, France) at 20 000rpm. Salt (0.5%) was added prior to the
94 addition of 6.5% of potato starch, 20% of skimmed milk (0.1% lipid), and 18% of the lipid mixtures. **The**
95 **composition of the model product was calculated in order to keep the total amount of added liquid**
96 **and lipids constant.** The lipids were stearic acid as free fatty acid (Stearic Acid ≥95%, Sigma-Aldrich, St.
97 Louis, Missouri, USA), oleic acid as free fatty acid (Oleic Acid 90%, Sigma-Aldrich, St. Louis, Missouri,
98 USA) and an EPA/DHA oil mix as triglycerides (EPAX 4535 TG/N, Epax Norway, Ålesund, Norway).
99 Stearic- and oleic acid had high purity (97% C18:0 and 93% C18:1 combined with 6% C18:2,

100 respectively) whereas the marine oil had a more diverse fatty acid profile with two major constituents
101 and multiple minors (51% C20:5, 37% C22:6, 1-5% C18:4, C20:4, C22:1, C22:5). The lipids were mixed
102 according to Figure 1, and will hereafter be denoted as “recipe 1”, “recipe 2”, etc. The lipids were
103 chosen based on melting points, in order to investigate the influence of the different phases of lipids
104 on the solubility of CO₂.

105 A total mixing time of 150s was applied. A control sample, recipe 8, was produced with extra milk, but
106 without the addition of lipids. Each recipe of mince was produced in two batches and mixed by hand
107 for 30s. The mince was stuffed in plastic casing ($\varnothing=60\text{mm}$, L=30-40cm), closed with metal clips and
108 heat-treated at 100°C for 1 hour. After the heat treatment, the mince product was cooled in the fridge
109 at $+4\pm 1^\circ\text{C}$ for 2-4 hours, prior to being frozen at $-23\pm 1^\circ\text{C}$ until packaging.

110 2.2 Packaging

111 The mince product was thawed for 48 hours at 4°C prior to being sliced in portions. The samples were
112 packaged ($101.3\text{g} \pm 4.1\text{g}$) in 300ml semi rigid crystalline polyethylene terephthalate (CPET) trays
113 (C2125-1B, Færch Plast, Holstebro, Denmark) using an automatic packaging machine (TL250,
114 Webomatic, Bochum, Germany). This gave a degree of filling of approximately $\frac{1}{3}$. The atmosphere was
115 evacuated (final vacuum pressure of 18mbar) and subsequently flushed with the gas mixture prior to
116 adhering the top film of a 40 μm combination of polyethylene (PE), ethylene vinyl alcohol (EVOH),
117 polyamide (PA), and polyethylene terephthalate (Topaz B-440 AF, Plastopil, Almere, The Netherlands).
118 Food grade CO₂ and N₂ was mixed using a gas mixer (MAP Mix 9000, Dansensor, Ringsted, Denmark)
119 to obtain pre-set packaging gas mixtures of 35% CO₂, 50% CO₂, or 70% CO₂ all balanced with N₂.
120 Hereafter referred to as 35/65, 50/50, and 70/30. Oxygen transmission rate (OTR) was 66-78cm³ x
121 25 μm^2 x 24h¹ x bar¹ at 23°C for the tray and 2.5cm³ x 40 μm^2 x 24h¹ x atm¹ at 23°C for the cover
122 film.

123 After packaging, the trays were stored at 0°C ($0.6\pm 0.7^\circ\text{C}$), 8°C ($7.8\pm 0.5^\circ\text{C}$), or 20°C ($20.0\pm 0.3^\circ\text{C}$)
124 respectively, for 7 days.

125 2.3 Water content, lipid content, and fatty acid composition

126 The water content of all the groups was determined gravimetrically by drying the samples for 24 hours
127 at 105°C (ISO.6496, 1983). Lipids were extracted and total amount calculated gravimetrically from the
128 mince product as described by Bligh and Dyer (1959). Eight samples were taken from each recipe and
129 each sample was divided into two; one for analysis of water content and one for analysis of lipid
130 content. The fatty acid composition was analyzed as fatty acid methyl esters in the lipid extracts from
131 the fish mince samples and in the pure lipids. Fatty acid methyl esters were analyzed using gas
132 chromatography (GC) (Agilent 6850 GC-system, Waldbronn, Germany) equipped with a flame

133 ionization detector (FID) set to 310°C, on a polyethylene glycol column (HP-INNOWax, Agilent,
134 Waldbronn, Germany 30m × 250µm × 0.25µm). Helium was used a carrier gas and the oven
135 temperature was set to 210°C. Preparation of methyl esters of the samples was conducted as described
136 by Metcalfe et al. (1966).

137 2.4 Differential scanning calorimetry analysis

138 The pure fats and samples recipe 1 through 8 were used for differential scanning calorimetry (DSC)
139 analysis. DSC was performed at a cooling rate of - 5 °C min⁻¹ over a temperature range from 20 °C to -
140 70 °C and then from -70 °C to + 70 °C at a heating rate of + 5 °C min⁻¹ on a DSC1 (Mettler Toledo,
141 Schwerzenbach, Switzerland). Aluminum crucibles (40 µl) were filled with sample (29.57 ± 1.96 mg
142 for stearic acid, 30.54 ± 1.36 mg for oleic acid and 31.17 ± 1.60 mg for the model products) and
143 sealed. An empty crucible was used as reference.

144 The enthalpy changes during cooling and heating were recorded. A rescan of previously scanned
145 samples was performed to identify irreversible reactions. The results were obtained by StarE
146 software version 14.0 (Mettler Toledo, Schwerzenbach, Switzerland).

147 2.5 Headspace gas analysis

148 The headspace gas composition (O₂ and CO₂) was measured using an oxygen and carbon dioxide
149 analyzer (Checkmate 9900 analyzer, PBI-Dansensor, Ringsted, Denmark). 20ml of the headspace gas
150 was collected with a syringe after intrusion of the top film. Before measurement of the composition, a
151 rubber septum (Nordic Supply, Skodje, Norway) was placed onto the top foil in order to avoid rupture
152 and introduction of false atmosphere. The gas compositions was measured in empty trays immediately
153 after packaging and in all trays at the end of the storage period.

154 2.6 Headspace gas volume

155 The headspace gas volume (mL) was assessed every day from day 1 through 7 by submerging the trays
156 under water and measuring the buoyancy force using a texture analyzer (Stable Micro System Ltd, TA-
157 XT plus, Godalming, UK) as described by Rotabakk et al. (2007). The trays were submerged at a rate of
158 2mm/s for 30s and held submerged for 30s to stabilize. Buoyancy force was measured every 2s a total
159 of 10 times. An average of the measurements was used for the further analyses. All measurements
160 were corrected according to the actual atmospheric pressure. The product density was measured to
161 be 1.08kg/m³.

162 The concentration of absorbed CO₂ can be related to package volume changes as described by
163 Rotabakk et al. (2007):

$$164 \quad C_{CO_2}^{t=\infty} = \frac{1,000 \cdot P(V_g^{t=0} - V_g^{t=\infty}) \cdot MwCO_2}{R \cdot T \cdot W_f}$$

165 Where $C_{CO_2}^{t=\infty}$ is the total CO₂ (ppm) absorbed by the product, P is absolute pressure (Pa), V_g is gas
166 volume (m³) at start and at equilibrium, MwCO₂ is the molecular weight of CO₂, R is the gas constant,
167 T is the absolute temperature (K), and W_f is the weight of the product (kg).

168 According to Henry's law, once a sample has reached equilibrium with the surrounding gas, the amount
169 of CO₂ in the headspace is proportional to the amount of CO₂ absorbed in the sample (Schumpe et al.,
170 1982):

$$171 \quad P_{CO_2}^{t=\infty} = H_{CO_2,p} \cdot C_{CO_2}^{t=\infty}$$

172 Where $P_{CO_2}^{t=\infty}$ is the equilibrium partial pressure of CO₂ in the headspace gas (Pa), $H_{CO_2,p}$ is the
173 temperature dependent Henry's constant for CO₂ in the sample (Pa/ppm). **The absorption of CO₂, and
174 thus Henry's constant is dependent on the composition of the product used, as different components
175 have different absorption potential. Comparison of Henry's constant for different foods can thus only
176 be carried out using adjustments to standardize the obtained results. In the present study, three
177 different adjustment methods were tested with the use of different assumptions (absorption only in
178 the water content, absorption in water- and total lipid content, or absorption in the water and liquid
179 lipid content). Content of liquid lipids were calculated based on storage temperature and theoretical
180 melting point. Obtained Henry's constants were divided by the amount of absorptive content under
181 each of the three assumptions.**

182 2.7 Statistics

183 Statistical analyses, including outlier test, analysis of variance (ANOVA) and general linear modelling
184 (GLM) were performed using minitab 17.0 (Minitab, Coventry, UK). Outlier testing was performed
185 using Grubbs outlier test at level p<0.05. GLM was performed using Tukey's HSD test at level p<0.05.
186 Data are given as mean±standard deviation (SD) unless otherwise stated.

187 3 Results and discussion

188 GLM analyses showed all parameters (storage temperature, lipid profile, storage time and packaging
189 gas combination) as well as all of the interactions effects to be of significant influence on the amount
190 of estimated dissolved CO₂ and Henry's constant (p<0.001). Only looking at the main effects, the main
191 discriminant factor for amount of estimated dissolved CO₂ was found to be packaging gas combination
192 (F=116999) followed by storage temperature (F=30747), lipid type (F=3653), and finally storage time
193 (F=1041). Despite showing interaction effects, all parameters were tested **in combinations** using
194 ANOVA.

195 The model used to estimate absorption of CO₂ into the model product is based on the assumption
196 that true flexible packages were used (Rotabakk et al., 2007). In the present study, truly flexible
197 packages were not obtainable and thus semi rigid trays were used. Even though the original study
198 assume true flexibility in the set-up the model was tested using semi rigid trays, and good correlation
199 were seen between estimated absorption and absorption calculated based on Henry's constant. In
200 Rotabakk et al., (2007) some problems with under pressure were seen when using high degrees of
201 filling (48% or higher) combined with high initial CO₂ levels (above 75%). In the present study, the
202 degree of filling was approximately 33% and initial CO₂ levels never rose above 70%, thus both
203 parameters lower than the critical values from the original study by (Rotabakk et al., 2007).
204 Therefore, despite the breach of the underlying assumptions, the results are still valid under the
205 given circumstances.

206 3.1 Raw material

207 3.1.1 Lipid content, water content, and fatty acid composition

208 Silver smelt was chosen as raw material based on its excellent freeze-thaw stability, good water holding
209 capacity, and low natural lipid content (Hellevik et al., 2005). These properties allowed for a stable raw
210 material that would not change significantly during the storage period. One of the focuses of the
211 current study was to investigate the influence of added lipids on the solubility of CO₂. By choosing a
212 raw material with a low initial lipid content, the findings of the experiment is representative of the
213 added lipids and not to the fish itself.

214 No significant difference in total lipid content was found in recipe 1 through 6. Recipe 7 exhibited a
215 visible lipid loss that resulted in a significant lower lipid content ($p < 0.001$) as compared to recipe 1
216 through 6. Analysis of the sum of lipid and water content showed the eight recipes to be separated
217 into two significantly different groups. Group one contains recipe 1 through 6 and group two contains
218 recipe 7 and 8. The recipes within each group was not significantly different from each other (Table 1).

219 The experiment was designed to obtain model products with a predetermined fatty acid profile, but
220 analyses showed small deviation between planned and actual composition (Figure 1 and Table 1). The
221 deviation is probably due to inaccuracies during production, as well as impurities in the added lipids as
222 seen from the lipid profiles of the pure oils (Table 1).

223 3.1.2 Differential scanning calorimetry analysis

224 DSC was performed in order to establish melting point/ranges of all samples. The results of multiple
225 DSC scans showed stearic acid to have a large change in energy in accordance with a phase transition,
226 confirming the expected melting point to be 75-80°C (data not shown). The marine oil was a mix of
227 multiple fatty acids, with the main constituents being EPA and DHA. This was evident in the analyses

228 that showed a wider range of phase transitions temperatures, as was expected with the sample being
229 a mixture. The entire range of the melting temperatures was outside the range of storage
230 temperatures, and thus not influential on the model product during storage. The pure oleic acid was
231 found to contain small amounts of linoleic acid in addition to the oleic acid. These findings was
232 confirmed by the DSC analysis, which showed two separate peaks at -8°C and +18°C (Figure 2A),
233 respectively. The +18°C peak representing the oleic acid, is very close to the storage temperature of
234 20°C. Furthermore, the scans shows that the full phase transition has not taken place before reaching
235 approximately 25°C. This shows that the oleic acid would not be in a complete liquid state during
236 storage, even at a storage temperature of 20°C.

237 3.2 Solubility of CO₂ in the fish model product

238 The relationship between the recipes and amount of dissolved CO₂ is rather complex, but certain
239 observations apply in general. The samples containing a pure marine oil (recipe 7) is always
240 insignificantly different from the control sample (recipe 8) with few exceptions. Results from 70/30
241 (Figure 3) are good representatives to the trends seen for samples packed with 50/50 and 35/65 (data
242 not shown). The solubility of CO₂ in fish has previously been found to be significantly dependent on
243 the total amount of water and lipid (Sivertsvik *et al.*, 2004). This correlates with recipe 7 and 8 having
244 no significant difference in sum content of lipid and water, while being significantly different from the
245 other recipes (Table 1 and Figure 3). It is believed that higher water and lipid content would lead to
246 higher amounts of dissolved CO₂ (Sivertsvik *et al.*, 2004). In the present study, samples containing least
247 water and lipid (recipe 7 and 8) had the significantly highest amount of dissolved CO₂, regardless of
248 packaging gas combination, storage time, and storage temperature (p<0.001). This indicates that the
249 *physical state* of the liquids (water and lipid) is more influential on the solubility than the *amount*. This
250 is confirmed by the finding of Devlieghere *et al.* (1998a) indicating that CO₂ mostly dissolves in liquid
251 lipid. This, in turn, explains why the samples containing 50% marine oil in the mixture (recipe 2 and 3)
252 was not significantly different (Figure 3), as the main influence on solubility is from the liquid marine
253 oil. This is further strengthened by the fact that the samples without liquid lipids (types 5, 6 and 1)
254 reached the lowest levels of dissolved CO₂ (Figure 3). The use of oleic- and stearic acid was included to
255 investigate this effect. Oleic- and stearic acid was chosen based on the differences in the expected
256 melting points, +13°C and +69°C, respectively (McMurry and Simanek, 2007). It was believed that
257 melting points above and below storage temperatures would result in different amounts of dissolved
258 CO₂ depending on the storage temperature. However, the samples containing pure oleic- or stearic
259 acid (recipe 6 and 5) showed no differences in dissolved amounts, regardless of temperature. Looking
260 at the DSC results, a change in energy was observed in the range from -5 to +15°C, indicating a phase
261 transition in this range (Figure 2C). This transition is ascribed to be the content of water. The analysis

262 was performed using a temperature increase rate of 5°C/min. This high rate of increase explains the
263 displacement of the water transition from the expected value of 0°C. When looking at the results for
264 recipe 6, the water-phase transition peak is shouldered by a smaller peak at around +16°C, resulting
265 from the content of oleic acid (Figure 2D). This shows that the lipids within the sample would be liquid
266 or at least semi-liquid when stored over longer periods at 20°C. This should lead to a potential for
267 increased uptake of CO₂ contradictory to the results observed for amount of dissolved CO₂ in the
268 current study. **The reason for this inconsistency is not understood.**

269 A better way to compare the solubility of CO₂ in different samples is to use Henry's constant. Henry's
270 constant is calculated using the concentration of CO₂ in the headspace gas *and* in the sample. **Thus,**
271 **unlike amount of absorbed CO₂, Henry's constant is independent of the gas composition of the**
272 **packaging gas (Table 2).** It has been customary to standardize Henry's constants of samples based on
273 the water content alone. This is done based on the assumption that CO₂ dissolves mainly in the water
274 phase (Meredith et al., 2014; Rotabakk et al., 2010). However, as mentioned, it has been found that
275 the solubility of CO₂ is dependent on the amount of both water and lipid (Jakobsen et al., 2009;
276 Rotabakk, 2013; Sivertsvik et al., 2004). Furthermore, (Gill, 1988) established that whereas the
277 solubility in water decreased with increasing temperatures, the solubility of CO₂ in lipid increased with
278 increasing temperatures up to a certain point depending on the fat source. This effect was ascribed to
279 the melting of the lipids. This indicates that the CO₂ is more prone to dissolve in liquid lipids rather
280 than solid lipids. It is usual to assume that Henry's constant for a food product can be calculated based
281 on Henry's constant for pure water and the water content of the product (Meredith et al., 2014). When
282 doing so, we find that the theoretical Henry's constant is a good approximation to the one measured
283 (data not shown) for all samples only containing solid lipids. On the other hand, samples containing
284 liquid lipids, that is all samples with some percentage of marine oil (recipe 2, 3, 4, and 7) and samples
285 with oleic acid when stored at 20°C (recipe 1 and 6), show the theoretical value to be a poor
286 representative of the actually measured value of Henry's constant. This indicates that the proper way
287 to present Henry's constant is to adjust for the content of water and *liquid* lipid. This further highlights
288 the influence of the relationship between lipids, melting points and storage temperatures, unlike what
289 was seen in the results for absorbed amount of CO₂ (Figure 3). All mentioned adjustment methods are
290 presented in Table 2. The choice of adjustment is further supported by the fact that adjustment based
291 on the water content or the sum of water and total lipids together reveals questionable results with
292 Henry's constants lower than those of water (30.3 Pa/ppm at 0°C, 39.9 Pa/ppm at 8°C, and 57.6
293 Pa/ppm at 20°C, respectively (Caroll *et al.*, 1991)).

294 Samples stored at 0°C revealed Henry's constants ranging from 31.9±2.9 Pa/ppm to 49.0±2.2 Pa/ppm,
295 recipe 7 and 6, respectively (Figure 4). The results clearly shows the temperature dependency of
296 Henry's constant, with increasing Henry's constant with increasing temperature. Recipe 1, 2, 3, 4, 5, 7,

297 and 8 all show high linearity with changes in temperature ($R^2=0.89-1.00$), however this is not the case
298 for recipe 6 ($R^2=0.62$). Increasing the temperature from 0 to 8°C, as expected, shows a significant
299 increase in Henry's constant. A further temperature increase does not result in further increase in
300 Henry's constant. This is due to the partial melting of the lipids changing the product composition. This
301 correlates perfectly with total content of water and liquid lipid (Table 1), showing that the solubility of
302 CO₂ in food is highly influenced by the composition of the fatty acids. Previous studies have reported
303 Henry's constants for multiple food products including several fish species. Sivertsvik *et al.* (2004)
304 found Henry's constant for a variety of raw fish fillets at 0°C to be in the range of 41.8±4.7 Pa/ppm to
305 49.1±5.2 Pa/ppm, which is similar to the majority of the results obtained in the present study. Fish
306 samples are not normally stored at temperatures as high as 8° or 20°C, and results are therefore not
307 presented for comparison.

308 The CO₂ level in the headspace immediately after packing was found to be 69.3±0.4, 50.2±0.3, and
309 35.6±0.3% CO₂, for 70/30, 50/50, and 35/65, respectively. The O₂ level was low for all samples
310 (0.1±0.2%), indicating that sufficient evacuation of the headspace was achieved.

311 As expected the packaging gas composition had a highly significant influence on the equilibrium CO₂
312 concentration in the headspace. Similar results was seen for dissolved CO₂ (Table 2). Solubility of CO₂
313 increased for all combinations of parameters with increasing initial CO₂ concentration. These findings
314 is supported by several other studies, including Rotabakk (2013), Rotabakk *et al.* (2008), and Sivertsvik
315 *et al.* (2004). A similar relationship as of packaging gas combination can be seen for the influence of
316 storage temperature. An increase from 0°C to 8°C or 20°C significantly lowered the amount of dissolved
317 CO₂ and increased Henry's constants in all samples, regardless of other parameters. These findings
318 agrees with results of previous studies including Rotabakk (2013).

319 Packaging gas composition had a significant influence on how the samples developed throughout the
320 storage period ($p<0.001$). Samples packed in both 50/50 and 70/30 showed a significant increase in
321 amount of dissolved CO₂ between measurements at 24 and 48 hours of storage ($p<0.04$), with few
322 exceptions. For the samples packed with 35/65, an increase in dissolved CO₂ concentration was not
323 observed until between 48 and 72 hours of storage. Except for the difference in the onset of
324 equilibrium, samples packed with 70/30 (Figure 3) are a good representation to the trends seen for
325 samples packed with 50/50 and 35/65 (data not shown). As for all equilibrium reactions, the dissolution
326 of CO₂ is driven by the differences in CO₂ concentration within the fish and in the gas phase (Sivertsvik
327 *et al.*, 2004). This explains the slower uptake of CO₂ in the 35/65 samples. The majority of the samples
328 showed a constant level of estimated dissolved amount of CO₂ after 96 hours of storage. This shows
329 that equilibrium has been reached after 4 days of storage. For some samples, equilibrium is reached
330 even earlier. These findings are in agreement with the findings of Sivertsvik and Jensen (2005) and

331 Sivertsvik *et al.* (2004), who found MA packed fish and meat products reached equilibrium after 3 to 4
332 days of storage.

333 To the best of our knowledge, this is the first study to measure the concentration of dissolved CO₂ in a
334 fish product as a function of time using different gaseous combination. However, Meredith *et al.* (2014)
335 performed a storage study on the effect of MAP of poultry fillets on CO₂ concentration in the meat.
336 They showed that samples with similar gaseous combination had an increase in amount of dissolved
337 CO₂ for the first 2-4 days where after equilibrium was reached. This is in agreement with the findings
338 in this study. At the end of the storage period, the CO₂ concentration in the chicken fillets reached
339 levels similar to those observed in the present study.

340
341 *Studies have showed that lipid composition of salmon muscle varies with feed type (organic or*
342 *conventional) (Lerfall *et al.*, 2016), breeding method (farmed or wild) as well as season (Hamilton *et*
343 *al.*, 2005), indicating that even seemingly similar products can be highly different when it comes to the*
344 *use of MAP. Therefore, the results of this study concludes* that solubility of CO₂ in a seafood model
345 product with added lipids is highly dependent on storage temperature and MA gas composition. *And*
346 *more* importantly, the solubility of CO₂ is correlated with the sum of liquid (water and liquid fat)
347 showing that the solubility of CO₂ is more dependent on the state of- rather than the type of
348 constituents. Lastly, this study showed that measurements of dissolved concentration of CO₂ is an
349 unsuitable measure for a comparison of solubility between days, treatments and/or samples. Henry's
350 constant gives a better basis for comparison. *These findings explain why previous studies on the*
351 *solubility of CO₂ have had highly contradicting results. Furthermore, the findings stress the need for*
352 *the food industry to understand their products, as well as making individual adjustments in the use of*
353 *MAP based on specific products and conditions in order to obtain the optimal condition for the shelf*
354 *life prolongation for the foods.*

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Table 1 Lipid content, water content, and fatty acid composition of the eight different model products. Only fatty acids composing more than 5% of the total lipid content are included.

Sample	Lipid [%] (n=8)	Water [%] (n=8)	Sum lipid and water [%]	Sum water and liquid lipid [%]	Fatty acid main constituents
Recipe 1	18.8±1.0 ^a	64.6±0.4 ^b	83.5±1.1 ^a	64.6±0.4 ^{d,e}	C18:0 (60%) C18:1 (37%)
Recipe 2	19.8±1.6 ^a	63.8±0.8 ^b	83.8±1.3 ^a	73.8±0.8 ^b	C18:0 (57%) C20:5 (23%) C22:6 (15%)
Recipe 3	18.9±0.8 ^a	64.2±0.5 ^b	82.9±0.9 ^a	73.5±0.6 ^b	C18:1 (54%) C20:5 (21%) C22:6 (14%)
Recipe 4	19.4±0.5 ^a	64.0±0.2 ^b	83.3±0.5 ^a	70.4±0.2 ^c	C18:0 (36%) C18:1 (34%) C20:5 (14%) C22:6 (10%)
Recipe 5	18.5±0.7 ^a	64.6±0.5 ^b	83.2±1.1 ^a	64.6±0.5 ^d	C18:0 (99%)
Recipe 6	18.5±0.2 ^a	63.9±0.7 ^b	82.4±0.8 ^a	63.9±0.7 ^e	C18:1 (93%)
Recipe 7	14.5±0.5 ^b	64.1±0.5 ^b	78.3±0.6 ^b	78.3±0.6 ^a	C20:5 (50%) C22:6 (37%)
Recipe 8	0.6±0.4 ^c	78.1±0.3 ^a	78.9±0.3 ^b	78.1±0.3 ^a	C16:0 (32%) C18:1 (17%) C20:1 (12%) C22:6 (15%)

Different superscript (a,b,c,d,e) in each column indicate significant variation ($p < 0.05$) by one-way ANOVA and Tukey's pairwise comparison test.

Recipe 1: 50/50 oleic/stearic acid, recipe 2: 50/50 Stearic/DHA and EPA mix, recipe 3: 50/50 Oleic/DHA and EPA mix, recipe 4: 33/33/33 Oleic/Stearic/DHA and EPA mix, recipe 5: 100% stearic acid, recipe 6: 100% oleic acid, recipe 7: 100% DHA and EPA mix, and recipe 8: control.

Table 2 *Main effect of packaging gas composition, fatty acid profile, and storage temperature on equilibrium headspace gas composition, equilibrium concentration of dissolved CO₂ in the model product, and Henry's constant adjusted for content of water, content of water and lipid, and content of water and liquid lipid, respectively. Key results are elaborated in Figure 3 and 4*

	Headspace CO ₂ [%]	Equilibrium CO ₂ concentration [ppm]	Henry's constant ¹ [Pa ppm ⁻¹]	Henry's constant ² [Pa ppm ⁻¹]	Henry's constant ³ [Pa ppm ⁻¹]
35	25±3	706±140	57±17	46±15	51±159
50	32±39	954±166	53±14	43±11	48±12
70	45±4	1376±235	52±13	41±9	48±16
Recipe 1	35±9	899±260	63±14	48 ±11	60±10
Recipe 2	33±9	1020±314	51±10	39±8	45±9
Recipe 3	32±9	1013±316	52±10	40±8	43±6
Recipe 4	33±9	991±324	55±11	42±9	48±8
Recipe 5	34±9	964±295	56±11	43±9	56±11
Recipe 6	35±9	940±292	61±11	47±9	55±5
Recipe 7	34±9	1153±388	50±21	41±18	41±18
Recipe 8	35±9	1140±395	43±18	44±18	46±25
0	31±8	1182±339	41.4±6.1	33.0±4	39±8
8	34±9	1030±291	50.9±7.5	40.5±4	48±9
20	37±9	825±264	70.2±12.0	56.0±11	61±15

¹ Adjusted for water content

² Adjusted for water- and total lipid content

³ Adjusted for water- and liquid lipid content

Recipe 1: 50/50 oleic/stearic acid, recipe 2: 50/50 Stearic/DHA and EPA mix, recipe 3: 50/50 Oleic/DHA and EPA mix, recipe 4: 33/33/33 Oleic/Stearic/DHA and EPA mix, recipe 5: 100% stearic acid, recipe 6: 100% oleic acid, recipe 7: 100% DHA and EPA mix, and recipe 8: control.

Figure captions

Figure 1: Composition of lipid mixtures added to the fish model product recipe 1 through 7. All mixtures were added to a total of 18% added lipid in the final product. A control, recipe 8, without addition of external lipids was included in the experiment. Recipe 1: 50/50 oleic/stearic acid, recipe 2: 50/50 Stearic/DHA and EPA mix, recipe 3: 50/50 Oleic/DHA and EPA mix, recipe 4: 33/33/33 Oleic/Stearic/DHA and EPA mix, recipe 5: 100% stearic acid, recipe 6: 100% oleic acid, recipe 7: 100% DHA and EPA mix, and recipe 8: control.

Figure 2: DSC results for phase transition temperatures of pure oleic acid (A), pure stearic acid (B), and recipe 5 containing the addition of 100% pure stearic acid (C) and recipe 6 containing the addition of 100% oleic acid (D), regardless of transition energy.

Figure 3: Concentration of CO₂ [ppm] in samples recipe 1 through 8 packed with 70% CO₂ in packaging gas and stored at 0, 8, and 20°C. Error bars indicates SD. . Recipe 1: 50/50 oleic/stearic acid, recipe 2: 50/50 Stearic/DHA and EPA mix, recipe 3: 50/50 Oleic/DHA and EPA mix, recipe 4: 33/33/33 Oleic/Stearic/DHA and EPA mix, recipe 5: 100% stearic acid, recipe 6: 100% oleic acid, recipe 7: 100% DHA and EPA mix, and recipe 8: control.

*Figure 4: Henry's constant adjusted for water- and liquid lipid content for samples recipe 1 through 8 stored at 0°, 8°, and 20°C. Error bars indicates SD. * most of the recipe 8 (control) samples stored at 20°C collapsed during the storage period, leading to highly irregular results, thus error bars has been removed, however the column is included to indicate the mean value. Recipe 1: 50/50 oleic/stearic acid, recipe 2: 50/50 Stearic/DHA and EPA mix, recipe 3: 50/50 Oleic/DHA and EPA mix, recipe 4: 33/33/33 Oleic/Stearic/DHA and EPA mix, recipe 5: 100% stearic acid, recipe 6: 100% oleic acid, recipe 7: 100% DHA and EPA mix, and recipe 8: control.*

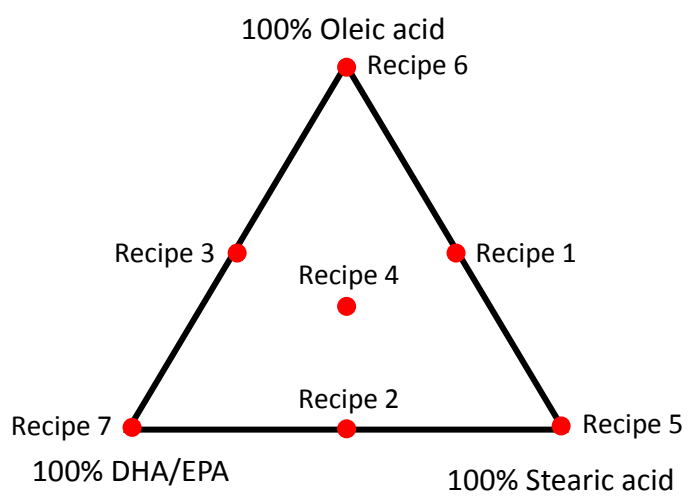


Figure 1.

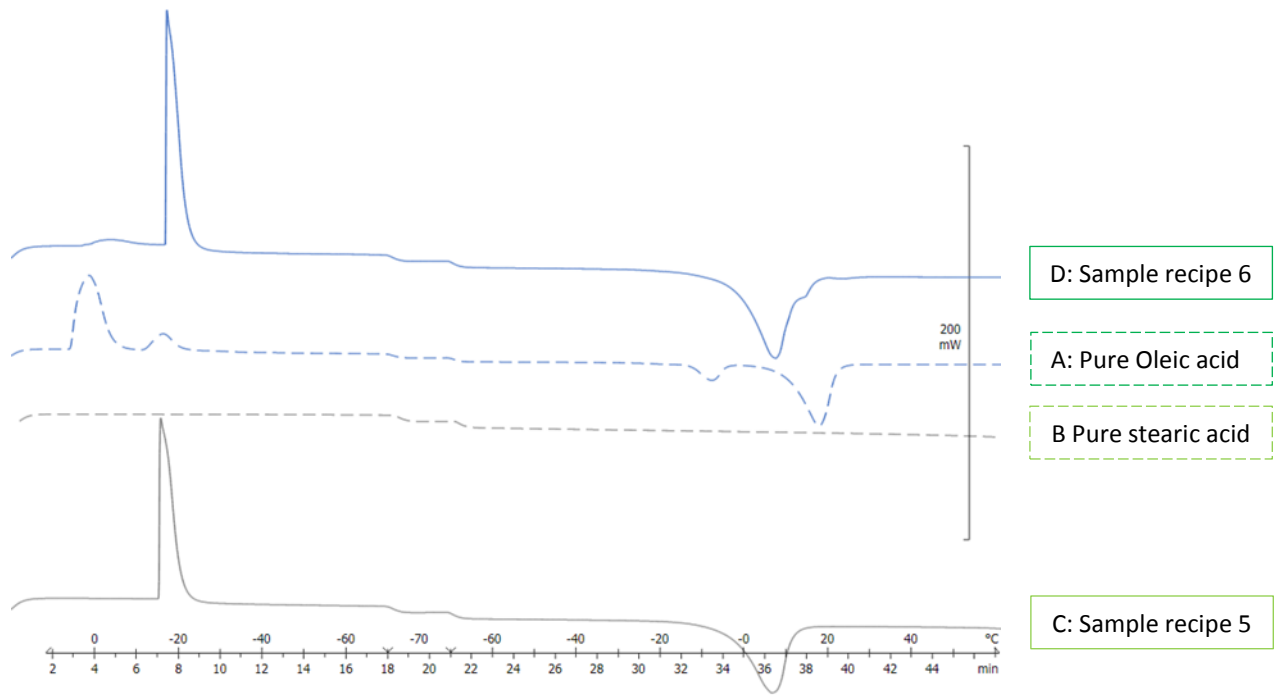


Figure 2.



Figure 3.

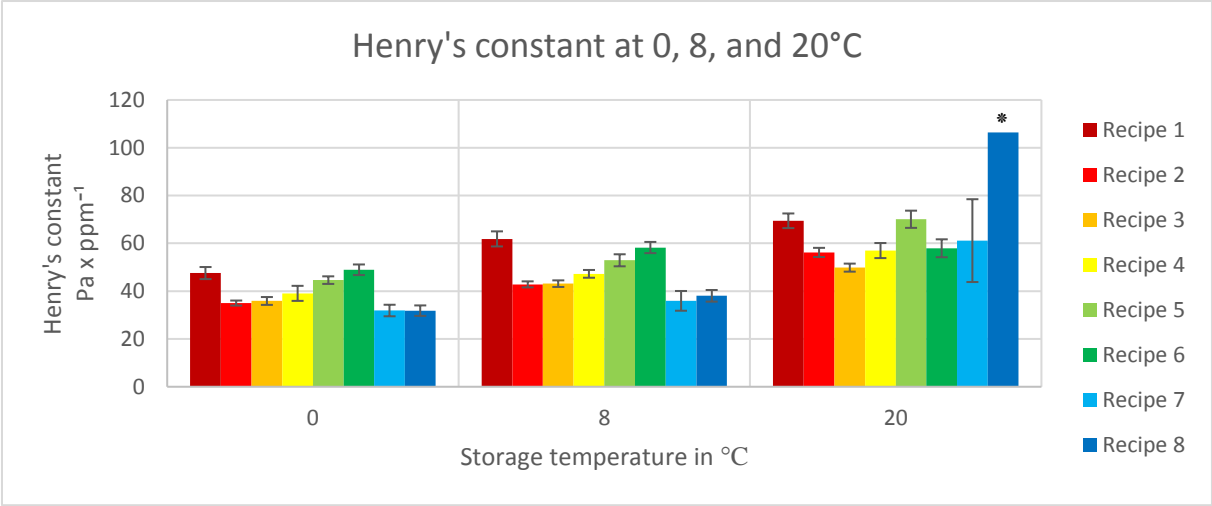


Figure 4.