

# Towards High Activity of Hydrogen production from Ammonia Borane over Efficient Non-noble Ni<sub>5</sub>P<sub>4</sub> Catalyst

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**Abstract:** Catalytic hydrolysis of ammonia borane has tremendous potential as an energy-efficient approach to supply hydrogen for energy vehicles and portable electronic devices. Herein, DFT calculation is first performed on electronic properties of Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> nanocatalysts. It is found that more electrons are transferred from Ni to P for Ni<sub>5</sub>P<sub>4</sub>, indicating that Ni<sub>5</sub>P<sub>4</sub> may show superior performance based on the electron effect. Therefore, Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> with high purity are synthesized by the phase-controlled thermal decomposition approach. Gratifyingly, the Ni<sub>5</sub>P<sub>4</sub> catalyst exhibits the as-expected better catalytic activity than that of Ni<sub>2</sub>P catalyst. It also shows low activation energy and good stability. Furthermore, the structures and morphologies of both catalysts are characterized by multi-techniques such as XRD, HRTEM and XPS. The better performance could be ascribed to the higher positive charge of Ni together with the stronger ensemble effect of P. The insights sheds new light on the design of efficient Ni-P catalysts for hydrogen generation.

**Keywords:** Ammonia borane; Catalytic hydrolysis; Electron transfer; Nickel phosphide

## Introduction

The ever-increasing demand for clean energy and concern for environment trigger the rapid development of alternative sustainable energy. Hydrogen, as a clean energy carrier, shows a significantly higher gravimetric energy density (120 kJ/g) than that of petroleum (44 kJ/g)[1]. It can be renewably produced from non-fossil feedstocks[2]. Although hydrogen shows obvious advantages such as energetic and clean, it still has drawbacks[3] in the storage, purification and production processes. Hydrogen storage is especially problematic, which imposes a scientific and technological challenge to researchers.

In order to address the above concerns, hydrogen generation from hydrogen storage materials offers the convenient, effective and cost-efficient approach[4-7]. The leading contender for chemical hydrogen-storage materials is ammonia-borane ( $\text{NH}_3\text{BH}_3$ , AB)[8-10]. It has the following advantages: 1) high hydrogen content (19.6 wt%) which is much higher than the targeted value (5.5 wt%) for the year 2020 set by the US Department of Energy; 2) low molecular weight (30.87 g/mol) and high volumetric density of 146 g/L; 3) high solubility in  $\text{H}_2\text{O}$ , long-term stability in aqueous solutions and air at room temperature and 4) non-toxicity. These characteristics have provoked tremendous research on AB hydrolysis.

Xu et al. first found that transition metals are active for AB hydrolysis[11]. Since then, many precious metals such as platinum[12, 13], rhodium[14, 15] and ruthenium[16] have been demonstrated to show high catalytic performance and low activation energy for AB hydrolysis. However, the high cost of precious metal has limited its commercial application. One scenario to solve this problem is to maximize the turnover frequency

of precious metal, such as reducing the nanoparticle size. For example, we systematically studied the size-dependence of Pt nanoparticle and greatly improved the performance[17]. Recently, Yan et al. employed the bottom-up precise method to synthesize stable platinum dimers on graphene, and achieved high specific rate of 2800 molH<sub>2</sub>/mol<sub>Pt</sub>/min at room temperature[18]. Another scenario is to use cost-effective non-precious metal to replace precious metal catalysts. To this end, nonprecious catalyst (e.g., nickel, iron, cobalt, copper) were reported to exhibit remarkable activities in the hydrolytic dehydrogenation of AB[19-22]. Fu et al. first reported that Ni<sub>2</sub>P could show good performance for AB hydrolysis[23]. It is noted that the nickel phosphate-based material could have different phases and may affect the performance of AB hydrolysis. Therefore, developing new nickel phosphate-based material and elucidate the effect of P on performance is highly desired to the design of efficient Ni-based catalyst for AB hydrolysis.

In this work, we first performed DFT calculation on electronic properties of Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> catalysts. Results show that more electrons can be transferred from Ni to P for Ni<sub>5</sub>P<sub>4</sub> catalyst. Based on the electronic effect for AB hydrolysis, it is estimated that Ni<sub>5</sub>P<sub>4</sub> may show superior performance. Therefore, Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> are experimentally synthesized by the phase-controlled thermal decomposition approach. Multi-techniques such as X-ray diffraction (XRD), transmission electron microscopy (TEM) and X-ray photoelectron spectroscopy (XPS) are employed to investigate the structure and morphology of the catalysts. Notably, the Ni<sub>5</sub>P<sub>4</sub> catalyst exhibits the as-expected better catalytic activity than that of Ni<sub>2</sub>P catalyst. This could be ascribed to the electronic effect (i.e., higher positive charge of Ni) together with the stronger ensemble effect of P. The results are of great referential importance to the design of efficient nickel phosphide catalysts for hydrogen generation.

## Experimental Section

### Chemicals

All chemicals were purchased from sinopharm chemical reagent unless otherwise indicated. The chemicals include ammonia borane ( $\text{NH}_3\cdot\text{BH}_3$ , 97%), nickel(II) acetylacetonate (95%), nickel(II) nitrate hexahydrate ( $\geq 98\%$ ), 1-octadecene (ODE, 95%), oleylamine (OAm, 70%), trioctylphosphine (TOP, 97%), hexane ( $\geq 99\%$ ), ethanol (96 vol%), cerium(IV) oxide (Sigma-Aldrich, 99.9995%) and carbon nanotube (CNano Technology Ltd). Deionized water (DI,  $18.2 \text{ M}\Omega\cdot\text{cm}$ ) was used in all experiments. All chemicals were used as received without further purification.

### Synthesis of $\text{Ni}_2\text{P}$ and $\text{Ni}_5\text{P}_4$ catalysts

In a typical process[24],  $\text{Ni}(\text{acac})_2$ , OAm (21.3 mmol) and ODE (14.1 mmol) were placed in a four-neck flask and vigorously stirred under argon atmosphere. The mixture was heated to  $120^\circ\text{C}$  and maintained for 30 min to remove dissolved oxygen and moisture. Afterwards, TOP was rapidly injected into the above solution, followed by heating to  $320^\circ\text{C}$  for 2 h. The products were subsequently obtained by adding excess ethanol and separated by centrifugation at 4000 rpm for 10 min. The black precipitate was washed with a mixture of hexane and ethanol for three times to remove excess surfactant and organic solvent, and then placed in vacuum at  $60^\circ\text{C}$  for 24 h. The molar ratios of the P : Ni precursor were 2.18 and 8.75 for  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$ , respectively.

### Synthesis of Ni, Ni/ $\text{CeO}_2$ and Ni/CNTs catalysts

The Ni/ $\text{CeO}_2$  and Ni/CNTs catalysts with same loading of 10wt% were prepared by incipient wetness impregnation method as follows. In a typical process, 1 g CNTs or  $\text{CeO}_2$  support was added in required volume of  $\text{Ni}(\text{NO}_3)_2$  aqueous solution at room

temperature. After vigorously stirring for 30 min, 5 wt% NaBH<sub>4</sub> solution was added to reduce Ni/CNTs or Ni/CeO<sub>2</sub> catalysts. The resulted products were filtered and washed with de-ionized H<sub>2</sub>O for three times to remove the by-products and residual ions. The as-obtained catalysts were then dried under vacuum at 50°C overnight. Ni catalyst is synthesized by NaBH<sub>4</sub> reduction of Ni(NO<sub>3</sub>)<sub>2</sub> aqueous solution at room temperature.

### **Catalyst characterization**

The crystal phases of Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> catalysts were determined by X-ray diffraction (XRD, Rigaku D/Max2550VB/PC, Cu K<sub>α</sub> radiation). The structure and shape of catalysts were obtained by high-resolution transmission electron microscopy (HRTEM) on a JEOL JSM-2010. The samples for TEM analysis were first prepared by sonicating in hexane. Subsequently, the mixture was deposited on an copper grid, which was slowly dried at ambient conditions. The binding energy of Ni was determined by x-ray photoelectron spectroscopy (XPS) analysis on a PHI5000Versa Probe spectrometer with monochromatic Al K<sub>α</sub> radiation (hν=1486.6 eV). Before XPS analysis, the samples were first stored under Ar atmosphere. The binding energy of C<sub>1s</sub> (284.6 eV) was used as a reference to correct the binding energy of the Ni-based catalysts. The spectra of Ni and P were deconvolution by XPSPEAK 4.1 with 80% Lorentzian-20% Gaussian peaks.

### **Catalytic testing**

In a typical water-displacement method, the catalytic activity of AB hydrolysis over Ni NP catalysts was evaluated by on-line recording of the hydrogen volume in a water-filled measuring cylinder system according to our previous report[17]. A weighed catalyst and Teflon-coated stirring bar were first placed in a three-necked glass container under stirring. This container inside water bath was connected via the gas

outlet to a water-filled measuring cylinder. The water bath was used to keenly change the reaction temperature. Subsequently, 5 mL AB solution (0.01g/mL) was introduced into the glass container by a syringe. Water was then displaced by the evolved hydrogen, the amount of which was determined by an electronic balance. The calculation of TOF is shown in supporting information. All experiments are well-repeated at least three times and the results are reproducible.

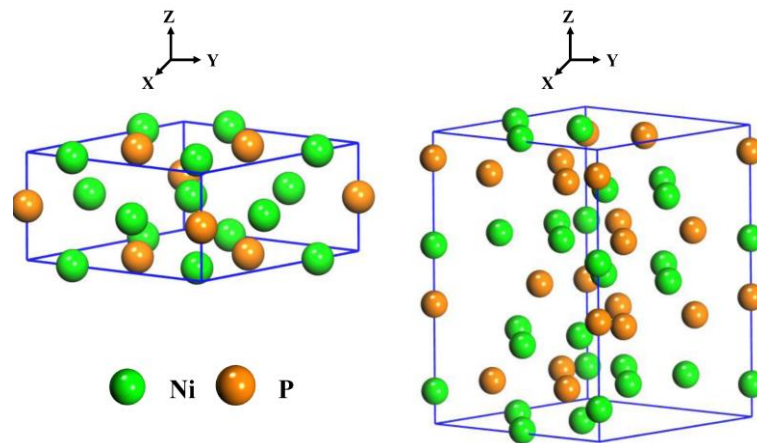
### **Calculation methods**

The density functional theory (DFT) calculation on the electronic properties of Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> catalysts was carried out with the DMol3 program package in Materials Studio. The unit cells of bulk Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> were built based on crystallographic data reported in literature[25]. The Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> geometry were optimized under three dimensional periodic boundary conditions to further refine the structure. Considering the electronic polarization effect, the double-numerical plus polarization (DNP) basis set with a real space cutoff radius of 4.5 Å and PW91 exchange-correlation functional were used according to literature[26]. The SCF tolerance was set as  $1.0 \times 10^{-6}$  Ha, and spin-unrestricted approach was used for all models. The atomic charges of the Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> were obtained by the popular charge analysis methods, i.e., the Mulliken analysis, which was based on projecting the occupied one-electron eigenstates onto a localized basis set[27, 28].

### **Results and discussion**

It was reported that Ni<sub>2</sub>P could show good performance for many reactions, such as AB hydrolysis[23, 29, 30], direct formic acid fuel cells[31] and hydrogen evolution reaction (HER)[24] because of the unique properties originated from the addition of P.

Herein, the electronic interaction between Ni and P is first investigated by DFT calculation. The geometries (Figure 1) of bulk  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$  model were built according to experimental lattice parameters[25]. For  $\text{Ni}_2\text{P}$ , the parameters are  $a=b=0.5859$  nm and  $c=0.3382$  nm. In contrast, the parameters for  $\text{Ni}_5\text{P}_4$  are  $a=b=0.679$  and  $c=1.099$ . Relatively large phosphorus is well accommodated using the trigonal prisms structure of this metal-rich phosphides. It can be seen from Table 1 that the optimized structural parameters of both  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$  coincide well with the experimental data and literature[25, 26, 32, 33], indicating the correctness of models.

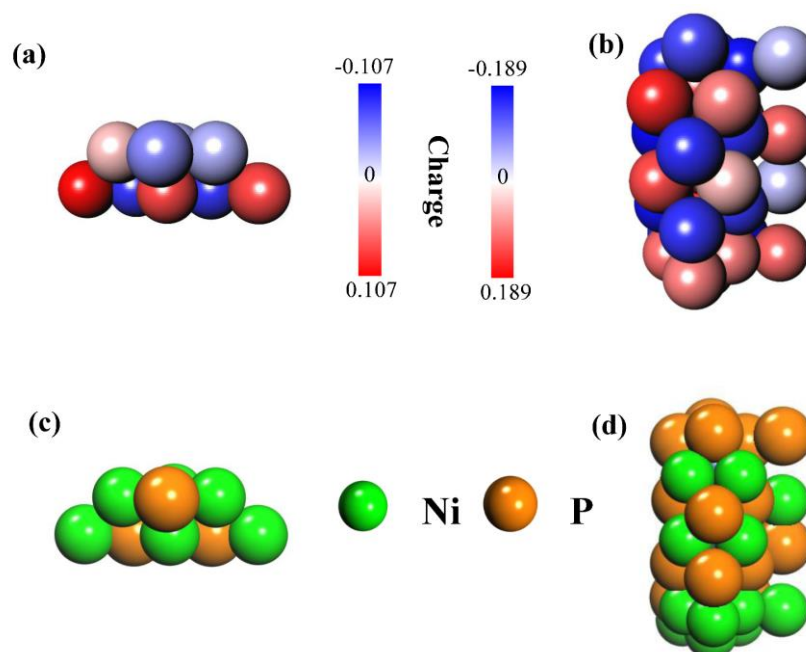


**Figure 1** Unit cell of  $\text{Ni}_2\text{P}$  (left) and  $\text{Ni}_5\text{P}_4$  (right) material.

**Table 1** Experimental and theoretical structural parameters of  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$ .

| Sample                  | nm | Theoretical | Experimental <sup>[25, 32, 33]</sup> |
|-------------------------|----|-------------|--------------------------------------|
| $\text{Ni}_2\text{P}$   | a  | 0.587       | 0.586                                |
| $\text{Ni}_2\text{P}$   | c  | 0.337       | 0.338                                |
| $\text{Ni}_5\text{P}_4$ | a  | 0.679       | 0.679                                |
| $\text{Ni}_5\text{P}_4$ | c  | 1.100       | 1.099                                |

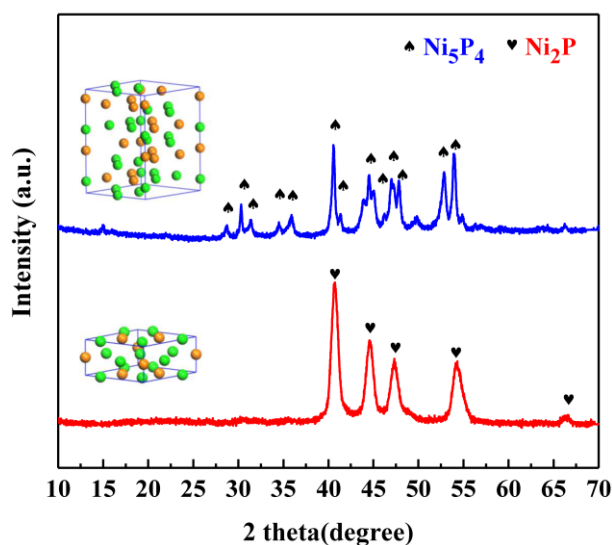
The Mulliken charge analysis is then performed, and the results are shown in Figure 2. For Ni<sub>2</sub>P the average charge per Ni atom after introduction of P is 0.038 e. This positive charge of Ni shows that there is electron transfer from Ni to P. In comparison, the average charge per Ni atom for Ni<sub>5</sub>P<sub>4</sub> is 0.119 e. This larger value shows that electron on Ni<sub>5</sub>P<sub>4</sub> is more easily to be transferred from Ni to P than on Ni<sub>2</sub>P. It is reported that the catalytic activity for AB hydrolysis can be greatly affected by the metal electronic properties[17]. For example, metal nanoparticle (e.g., Pt) that donates electron to support exhibits significantly increased hydrogen generation rate than Pt catalyst that receives electron. Therefore, based on this electronic effect, it is thus expected that Ni<sub>5</sub>P<sub>4</sub> material with more electron transfer from Ni to P may exhibit higher TOF (mol<sub>H<sub>2</sub></sub>/mol<sub>cat</sub>/min).



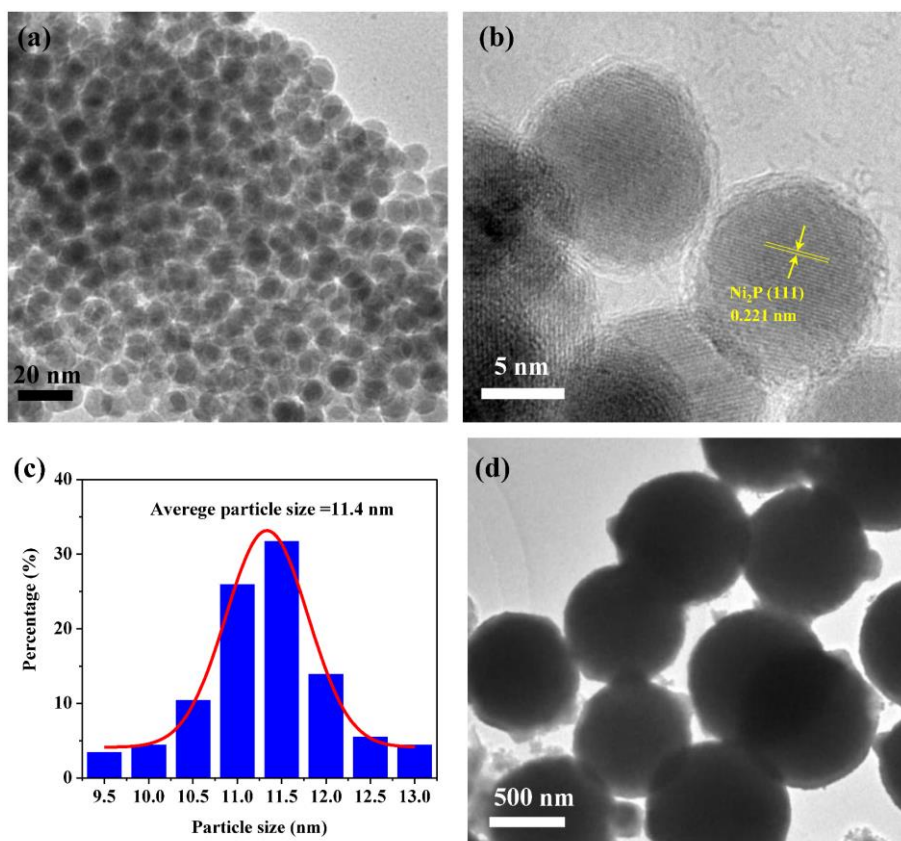
**Figure 2** Charge analysis of bulk Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> materials. The blue and red colors indicate the charge labeled in the color map, where blue and red value means receiving or donating electrons, respectively. The figure 2(c-d) are shown to distinguish the Ni and P atoms.



The crystalline phase structure and the purity of the as-synthesized nickel phosphide (i.e.,  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$ ) catalysts are characterized by XRD, as shown in Figure 3. When the P/Ni ratio is 2.18,  $\text{Ni}_2\text{P}$  phase with high purity was obtained. The intense diffraction peaks at 40.8, 44.7, 47.5, 54.4, 66.4 are attributed to the (111), (201), (210), (300), (310) crystal facets, respectively. These diffraction peaks are in accordance with the hexagonal structure of  $\text{Ni}_2\text{P}$  (PDF#03-065-3544). No extra peaks are clearly observed in this range, indicating the high purity of  $\text{Ni}_2\text{P}$  phase. Higher P/Ni ratio of 8.75 results in the presence of  $\text{Ni}_5\text{P}_4$  phase. The hexagonal structure of  $\text{Ni}_5\text{P}_4$  matches well with all diffraction peaks (PDF # 03-065-2075). The intense diffraction peaks at 28.8, 30.4, 31.5, 34.7, 36.1, 40.6, 41.4, 46.3, 47.0, 47.9, 49.9, 53.1 and 54.1 are attributed to the (103), (200), (201), (202), (104), (210), (211), (300), (301), (213), (006), (303) and (220) crystalline phases, respectively. No other obvious extraneous peaks exist, confirming the purity of crystal. These XRD results show that both of  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$  have high crystallinity and purity, which are required to elucidate the electronic effect and structure-performance relationship for AB hydrolysis.



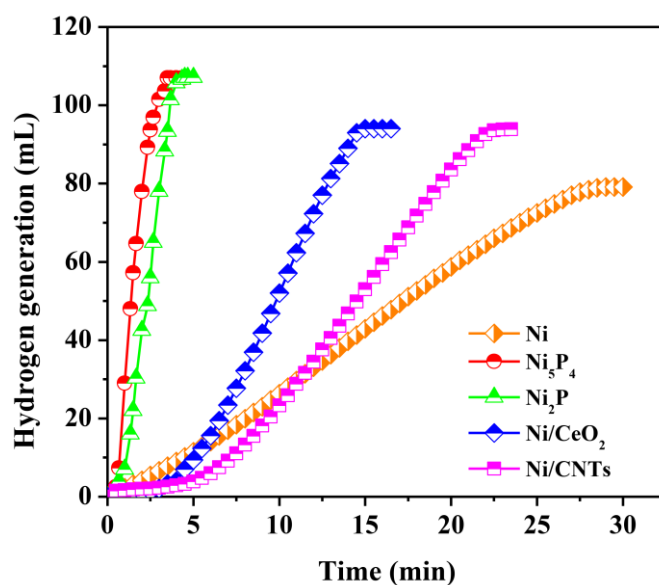
**Figure 3** XRD patterns of  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$  catalysts.



**Figure 4** Representative HRTEM images of nickel phosphide different phases of Ni<sub>2</sub>P (a-b) and Ni<sub>5</sub>P<sub>4</sub> (d), and particle size distribution of Ni<sub>2</sub>P catalyst (c).

Figure 4 and Figure S1-S2 show the representative TEM images of Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> catalysts. It can be seen that the Ni<sub>2</sub>P shows regular solid spherical shape with average particle size of ca. 11 nm. The HRTEM image (Fig. 4b) reveals that the fringe spacing is about 0.221nm. This corresponds to the (111) lattice plane of hexagonal Ni<sub>2</sub>P, which coincides well with the XRD results in Figure 3. Fig. 4d shows the morphology of the Ni<sub>5</sub>P<sub>4</sub> catalyst. It can be seen that only big solid spheres are obtained, and the average particle size is ca. 800 nm (Figure S3). This can be explained by the nickel phosphate formation mechanism[24]. In the synthesis process, nickel nanoclusters can be first formed using OAm as the reductant when the reaction temperature reaches 200°C. Subsequently, P precursor (i.e., TOP) can strongly adsorb on the surface of Ni, forming

the Ni-TOP complexes [24]. With the gradual increase of reaction temperature to 320°C, the phosphorus is formed by the breaking of P-C bond. The as-formed phosphorus can therefore diffuse into the Ni nanoclusters, forming Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> nanoparticles. When the Ni/P ratio is high (i.e., Ni<sub>2</sub>P), the inward diffusion of phosphorus atoms is larger than the outward diffusion, and thus generates small solid Ni<sub>2</sub>P nanoparticle. When the Ni/P ratio is smaller for Ni<sub>5</sub>P<sub>4</sub>, a similar diffusion speed of nickel and phosphorus is reached, resulting in steady state in all directions of the particle. Because of the high surface energy and intermolecular forces of the unstable solid nanoparticle, the aggregation of Ni<sub>5</sub>P<sub>4</sub> into solid spheres occurs. These results confirm that the crystal phase of nickel phosphide can be controlled by carefully modifying the Ni/P ratio.



**Figure 5** Catalytic activity of different Ni-based catalysts with same weight of 0.038g.

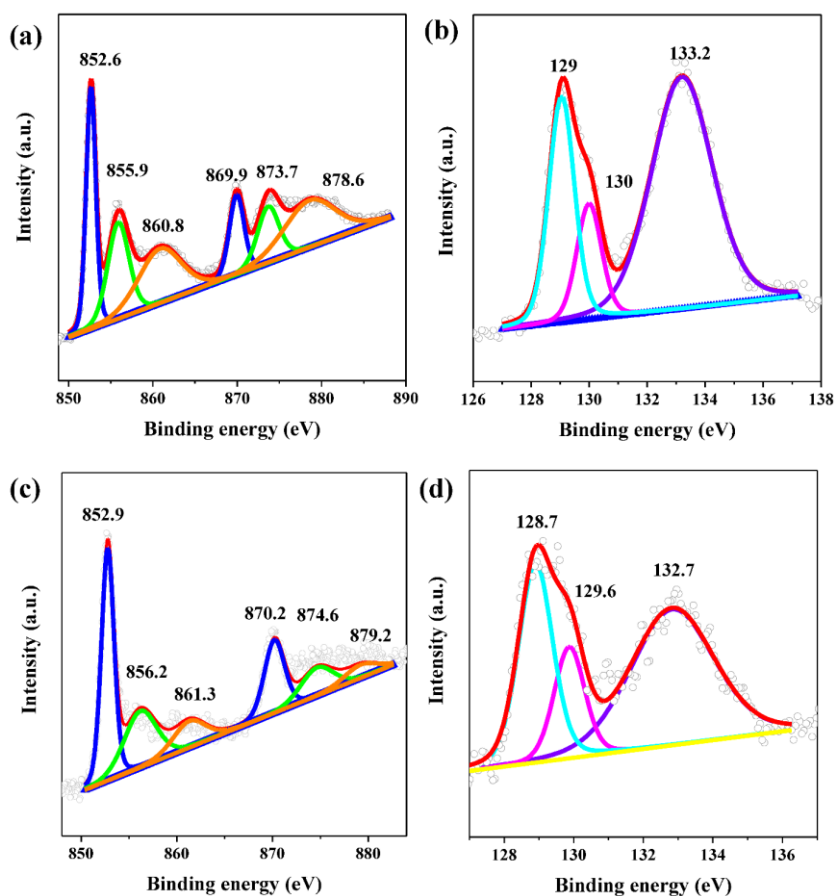
Reaction conditions: 25°C, C<sub>AB</sub>=0.01g/mL, V<sub>AB</sub>=5mL.

The catalytic performance of Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> catalysts are therefore tested for AB hydrolysis (Figure 5). AB hydrolysis reaction is depicted as the following equation,  $\text{NH}_3\text{BH}_3 + 4\text{H}_2\text{O} \rightarrow \text{NH}_4^+ + \text{B}(\text{OH})_4^- + 3\text{H}_2$ [20]. Therefore, the maximum value of 3mol

H<sub>2</sub> can be generated with 1 mol of NH<sub>3</sub>BH<sub>3</sub> for each experiment. It can be seen that only less than 100 mL of hydrogen can be generated in 14, 22 and 28 min for Ni/CeO<sub>2</sub>, Ni/CNTs and Ni catalyst, respectively. In sharp contrast, the Ni<sub>2</sub>P catalyst can generate total amount of hydrogen in ca. 3 min. Compared with Ni<sub>2</sub>P catalyst, Ni<sub>5</sub>P<sub>4</sub> shows as expected higher activity, with generation of all hydrogen in shorter time. The calculated TOF for Ni<sub>5</sub>P<sub>4</sub> and Ni<sub>2</sub>P is 23.5 and 6.3 mol<sub>H<sub>2</sub></sub>/min/mol<sub>cat</sub>, respectively.

Normally, smaller Ni<sub>x</sub>P<sub>y</sub> particle size leads to better performance. However, Ni<sub>5</sub>P<sub>4</sub> with larger particle size still shows higher TOF than Ni<sub>2</sub>P. Therefore, size effect should not be the dominate reason. The electronic properties of the two catalysts are further studied. The chemical states of Ni and P elements for Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> catalysts are studied by XPS. Figure 6a shows the Ni 2p<sub>3/2</sub> and Ni 2p<sub>1/2</sub> regions, which consist of spin-orbit doublets and shakeup satellite peaks. In the Ni 2p<sub>3/2</sub> region of Ni<sub>2</sub>P sample, the three peaks with binding energy (BE) of 852.6, 855.9 and 860.8 eV are ascribed to the Ni<sup>δ+</sup>[34, 35], Ni(II) from superficial oxidation of Ni<sub>2</sub>P[36] and satellite peak of Ni 2p<sub>3/2</sub>[37], respectively. In addition, the Ni<sup>δ+</sup> in Ni<sub>2</sub>P, oxidized Ni species and satellite peak of Ni 2p<sub>1/2</sub> region are found at 869.9, 873.7 and 878.6 eV. Compared with Ni<sub>2</sub>P, the three corresponding peaks of Ni 2p<sub>3/2</sub> are observed at 852.9, 856.2 and 861.3 eV for Ni<sub>5</sub>P<sub>4</sub>. It can be seen that there is positive shift of BE for each peak of Ni<sub>5</sub>P<sub>4</sub> catalyst. For example, the Ni<sup>δ+</sup> shifts from 852.6 to 852.9 eV for Ni<sub>5</sub>P<sub>4</sub> catalyst. This positive shift for Ni<sub>5</sub>P<sub>4</sub> shows that Ni donates more electron, which is in accordance with the DFT calculation in Figure 2. Figure 6b and 6d show the P 2p region of Ni<sub>2</sub>P and Ni<sub>5</sub>P<sub>4</sub> catalysts. For Ni<sub>2</sub>P catalyst, the peaks at 129.0 and 130.0 are assigned to P 2p<sub>1/2</sub> and P 2p<sub>3/2</sub> in Ni<sub>2</sub>P, respectively[38], and the peak at 133.2 eV is ascribed to oxidized P species. In comparison, the P 2p peaks of Ni<sub>5</sub>P<sub>4</sub> show negative shifts. The corresponding peaks are observed at 128.7, 129.6 and 132.7 eV. The negative shift of P2p peaks

together with positive shifts of Ni 2p peaks confirm the DFT calculation



**Figure 6** XPS spectra of Ni 2p and P 2p for Ni<sub>2</sub>P (a, b) and Ni<sub>5</sub>P<sub>4</sub> (c, d) catalysts.

results that more electron are transferred from Ni to P for Ni<sub>5</sub>P<sub>4</sub> catalyst. The electron-deficient metal sites are favor for the adsorption of B-H in AB molecule, forming and breaking M-H bond to generate H<sub>2</sub>. Therefore, this should be one reason for the enhanced catalytic activity for Ni<sub>5</sub>P<sub>4</sub> catalyst towards AB hydrolysis. Besides enhanced electron transfer on Ni<sub>5</sub>P<sub>4</sub> catalyst, it is worth noting that the ensemble effect of P could also be beneficial for improving the catalytic activity. The contents of P in Ni<sub>5</sub>P<sub>4</sub> (44 at% P) is actually larger than that in Ni<sub>2</sub>P (33 at% P). In addition, the Ni/P ratio determined from XPS is also quite similar to the stoichiometric ratio. Therefore, this ensemble effect reduces the number of Ni active sites, decreasing the energy cost

for H<sub>2</sub> removal from nickel phosphate catalyst.

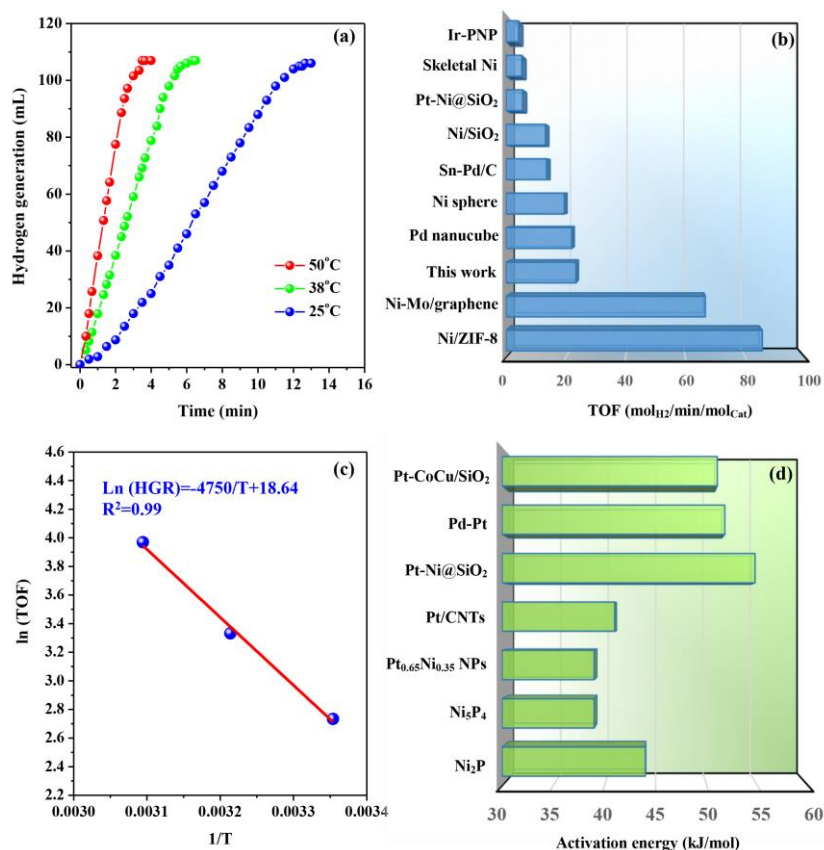
The catalytic activity of Ni<sub>5</sub>P<sub>4</sub> catalyst is subsequently evaluated at different temperature with smaller n<sub>Cat</sub>/n<sub>AB</sub> ratio of 0.02 (Figure 7a). With the increase of reaction temperature from 25 to 50 °C, the TOF can be further increased to 53 mol<sub>H2</sub>/min/mol<sub>cat</sub>. This observation agrees well with previously reported results that high temperature is favorable for the hydrogen generation in AB hydrolysis. Compared with literature (Figure 7b)[38-40], the TOF of Ni<sub>5</sub>P<sub>4</sub> at 25°C (Figure 5) is quite impressive. It is even higher than some of precious catalysts[41-44], such as Ir-PNP, Sn-Pd/C and Pt-Ni@SiO<sub>2</sub>. It should be noted increasing the n<sub>Cat</sub>/n<sub>AB</sub> ratio or changing AB concentration could further enhance the activity[23, 29]. However, the aim of this paper is to propose a strategy to modify catalytic performance by manipulating electron transfer for nickel phosphate catalyst. Therefore, further enhancing performance by other methods such as adding promoter, studying size effect or optimizing reaction conditions are interesting topics, which may be taken in our future study.

The temperature dependent TOF can be used to evaluate the activation energy (i.e., E<sub>a</sub>) by Arrhenius equation (3-1):

$$r = r_0 \exp\left(-\frac{E_a}{RT}\right) \quad (3-1)$$

where  $r$  is the TOF (mol<sub>H2</sub>/min/mol<sub>Cat</sub>), E<sub>a</sub> is the activation energy (kJ/mol), T is the absolute temperature (K) and R is the gas constant (8.3145J/mol/K). From Figure 7c, the calculated activation energy for Ni<sub>5</sub>P<sub>4</sub> is 39 kJ/mol, comparable or even smaller than some of reported precious catalysts in Figure 7d (e.g., Pt-Ni@SiO<sub>2</sub> of 54.76[45], Pd-Pt NPs of 51.77[46], Pt<sub>0.65</sub>Ni<sub>0.35</sub> of 39[47], Pt-CoCu@SiO<sub>2</sub> of 51.01 eV[41]). This

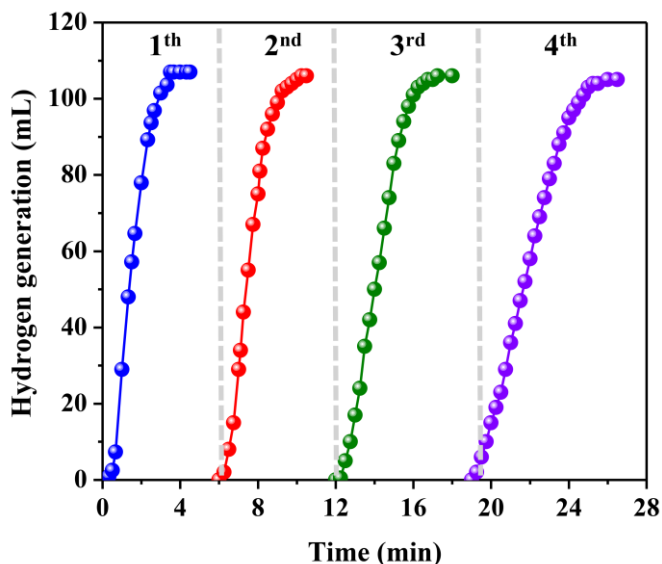
indicates the potential of this nickel phosphate catalyst for AB hydrolysis.



**Figure 7** Time courses for H<sub>2</sub> production from hydrolysis of AB using Ni<sub>5</sub>P<sub>4</sub> at low  $n_{\text{cat}}/n_{\text{AB}}$  of 0.02 (a), Arrhenius plot of ln (TOF) versus 1/T (c), comparison of the TOF (b) and activation energy (d) with different reported catalysts.

The durability test of Ni<sub>5</sub>P<sub>4</sub> catalyst is performed at room temperature, and shown in Figure 8. It is conducted by the addition of a new proportion of AB solution when the previous run was completed. It can be seen that the Ni<sub>5</sub>P<sub>4</sub> catalyst shows good stability and reusability. The high activity after fourth test is still retained. The relatively slower hydrogen generation rate is observed, which could be ascribed to the slight particle agglomeration (Figure S4). This phenomenon is also observed for Ni<sub>2</sub>P catalyst[23]. From the above computational and experimental results, it can be seen that manipulating the electron transfer and employing the ensemble effect of P can be effective strategies to enhance the performance of nickel phosphate catalyst for AB

hydrolysis. The results reported herein may pave the way for the rational design of highly efficient nickel phosphate-based catalysts for hydrogen generation.



**Figure 8** Cycle stability test of  $\text{Ni}_5\text{P}_4$  for hydrogen generation with the weight of 0.038g.

Reaction conditions:  $25^\circ\text{C}$ ,  $C_{\text{AB}}=0.01\text{g/mL}$ ,  $V_{\text{AB}}=5\text{mL}$ .

## Conclusions

In summary, the  $\text{Ni}_2\text{P}$  and  $\text{Ni}_5\text{P}_4$  are synthesized by the phase-controlled thermal decomposition approach and characterized by multi-techniques such as XRD, TEM, XPS. By both DFT calculation and experimental methods, the facilitated electron transfer from Ni to P for  $\text{Ni}_5\text{P}_4$  than  $\text{Ni}_2\text{P}$  is demonstrated. It is found that  $\text{Ni}_5\text{P}_4$  catalyst shows impressive catalytic hydrogen evolution rate for ammonia-borane hydrolysis, which is higher than that of  $\text{Ni}_2\text{P}$  catalyst. The activation energy of the  $\text{Ni}_5\text{P}_4$  catalyst for the hydrolysis of AB is calculated to be 39 kJ/mol, smaller than part of precious metal catalyst. This could be ascribed to the higher positive charge of Ni together with the stronger ensemble effect.



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