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classdef InjectionObj < handle
%InjectionObj. Injection Object
% InjectionObj represents a injection point into the well structure.
% It
% includes viscosity blending calculations according Cragoe and ASTM
% D7152.
%
% Properties
% - Qd          : flowrate diluent @local conditions [m3/d]
% - Qo          : flowrate oil @local conditions [m3/d]
% - Qw          : flowrate water @local conditions [m3/d]
% - Tb          : blending temperature [C]
% - drho        : density diluent [kg/m3]
% - orho        : density oil [kg/m3]
% - mrT         : reference matrix temperature [C]
% - mrmu        : reference matrix viscosity [cP or
cSt]
% - BlendingMethod : blending method
% - CragoeA       : Cragoe's method A coefficient
% - CragoeB       : Cragoe's method B coefficient
% - bmrmu         :
% - bmrT          :
%
% Dependent properties
% - status        : programming property (to be used in further
versions)
% - brho          : density blend [kg/m3]
% - bmu           : viscosity blend [cP]
% - bSG           : specific gravity blend [-]
% - WC            : water cut [-]
%
% Methods
% - BlendingReference
% calculation of two referencial matrices including viscosity
at 5
% different temperature values.
%
%-----
% Development
% By: Ruben Ensalcado
% 2015
% Rev 00 151216 original release
% Rev 01 151230 description change: Qd, Qo, Qw
% inclusion property: bmrmu, bmrT
% inclusion method: BlendingReference
%
% Developer notes:
% - mrmu : row orientation per reference
% - mrT : row orientation per reference
%
properties
Qo

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        Qd
        Qw
        Tb
        mrT
        mrmu
        bmmu
        bmrT
        orho
        drho
        BlendingMethod
        CragoeA
        CragoeB
    end

    properties (Dependent = true)
        status
        bmu
        brho
        bSG
        WC
        wt
    end

    properties (Hidden = true, Constant = true)
        wrho = 1000;          %P = 1 atm, T = 4 C
    end

    methods (Hidden = true)
        % -- initialization method --

        function BL = InjectionObj
            BL.BlendingMethod = 'astm_d7152';
            BL.CragoeA = 5e-2;
            BL.CragoeB = 1e3*log(20);
        end
    end

    methods
        % -- error verification methods --

        function set.BlendingMethod(BL, umethod)
            if strcmpi(umethod, 'cragoe') ||
                strcmpi(umethod, 'astm_d7152')
                BL.BlendingMethod = umethod;
            else
                error('InjectionObj:BadArgument', ...
                    'The available methods are: CRAGOE and
ASTM_D7152!')
            end
        end

        function set.mrmu(BL, umrmu)
            if size(umrmu, 2) == 2
                BL.mrmu = umrmu;
            end
        end
    end

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        else
            error('InjectionObj:BadArgument', ...
                'mrmu must be a matrix nx2, where n is the
number of fluids!')
        end
    end

    function set.mrT(BL, umrT)
        if size(umrT, 2) == 2
            BL.mrT = umrT;
        else
            error('InjectionObj:BadArgument', ...
                'mrT must be a matrix nx2, including the
reference temperature value!')
        end
    end

    function set.Tb(BL, uTb)
        if size(uTb, 1) == 1 && size(uTb, 2) == 1
            BL.Tb = uTb;
        else
            error('InjectionObj:BadArgument', ...
                'Tb must be a single temperature value!')
        end
    end
end

methods
    % -- dependent properties --

    function status = get.status(BL)
        %Status. Independent property verification

        req = zeros(4, 1);

        req(1) = isempty(BL.wt);
        req(2) = isempty(BL.mrT);
        req(3) = isempty(BL.Tb);
        req(4) = isempty(BL.mrmu);

        if all(~req)
            status = true;
        else
            status = false;
        end
    end

    function bmu = get.bmu(BL)
        %DynamicViscosity. (blend)
        %Units
        % bmu : cP

        switch lower(BL.BlendingMethod)
            case 'cragoe'

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        bmu = BlendingCragoe(BL);
    case 'astm_d7152'
        bmu = BlendingASTM_D7152(BL);
    end
end

function WC = get.WC(BL)
    %WaterCut.
    %Units
    % Qw : m3/d
    % Qo : m3/d
    % Qd : m3/d

    WC = (BL.Qw)/(BL.Qo + BL.Qd + BL.Qw);
end

function bSG = get.bSG(BL)
    %SpecificGravity. (blend) Definition
    %Units
    % brho : kg/m3
    % wtho : kg/m3

    bSG = BL.brho/BL.wrho;
end

function brho = get.brho(BL)
    %Density. (blend) Mass balance
    %Units
    % drho : kg/m3
    % orho : kg/m3
    % Qo : m3/d
    % Qd : m3/d
    % brho : kg/m3

    brho = (BL.orho*BL.Qo + BL.drho*BL.Qd)/(BL.Qo + BL.Qd);
end

function wt = get.wt(BL)
    %WeightFraction.
    %Units
    % drho : kg/m3
    % orho : kg/m3
    % Qo : m3/d
    % Qd : m3/d

    wt = zeros(2, 1);
    wt(1) = BL.orho*BL.Qo/(BL.orho*BL.Qo + BL.drho*BL.Qd);
    wt(2) = 1 - wt(1);
end

end

methods
    function BlendingReference(BL)

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        %BlendingReference. Reference for blend viscosity
        %Units
        % Tb      : C
        % bmrT    : C
        % bmrmu    : cP

        T0 = BL.Tb;
        BL.bmrmu = zeros(5, 1);
        BL.bmrT = linspace(T0 - 10, T0 + 10, 5)';

        for i = 1:5
            BL.Tb = BL.bmrT(i);
            BL.bmrmu(i) = BL.bmu;
        end

        BL.Tb = T0;
    end

end

methods (Access = protected, Hidden = true)
    % -- viscosity calculation methods --

    function bmu = BlendingCragoe(BL)
        %BlendingCragoe. Blending according Cragoe's method (1933)
        %Units
        % vscm : cP
        % bnu  : cP
        % T    : C

        A = BL.CragoeA;
        B = BL.CragoeB;

        vscm = BL.mrmu;
        lij = B./log(vscm/A);
        lbm = lij(:, 1) + (BL.Tb - BL.mrT(:, 1)).*(lij(:, 2) -
lij(:, 1))./...
                                (BL.mrT(:, 2) - BL.mrT(:, 1));
        lmx = sum(BL.wt.*lbm);
        bmu = A*exp(B/lmx);
    end

    function bnu = BlendingASTM_D7152(BL)
        %BlendingASTM_D7152. Blending according ASTM D7152 (2011)
        %Units
        % vscm : cSt
        % bmu  : cSt
        % T    : C

        vscm = BL.mrmu;
        zij = vscm + 0.7 + exp(-1.47 - 1.84*vscm - 0.51*vscm.^2);
        wij = log10(log10(zij));
        Tij = log10(BL.mrT + 273.15);

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Ttb = log10(BL.Tb + 273.15);
mnv = (Tij(:, 2) - Tij(:, 1))./(wij(:, 2) - wij(:, 1));

wb = (Ttb + sum(BL.wt.*(mnv.*wij(:, 1)-Tij(:, 1))))/
(sum(BL.wt.*mnv));
zb = 10^(10^wb) - 0.7;

bnu = zb - exp(-0.7487 - 3.295*zb + 0.6119*zb^2 -
0.3191*zb^3);
    end
end
end
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